

DE/AFS/SF cc: B. Reger S Van Zanat TFRO

October 9, 2006

Mr. Mike Simon
Stationary Source Program Manager
Idaho Department of Health and Welfare
Division of Environmental Quality
1410 North Hilton
Boise, Idaho 83706

ility ID No .: 031 -00026 RECEIVED

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Department of Environmental Quality
State Air Program

Logged:

Re:

Sinclair Burley Products Terminal (Sinclair)

Sinclair Transportation Company

Tier 1 Operating Permit No. T1-030413 / Tier 2 Operating Permit No. T2-030419

Permit No.: 12

AIRS Facility No. 031-00026

Transmittal of Tier 1 and Tier 2 Operating Permit Application Renewals

Mr. Simon:

Sinclair is currently operating under the provisions of its Tier 1 operating permit as revised on January 13, 2004. The current Tier 1 permit expires on July 4, 2007. With this correspondence, Sinclair is formally submitting its application to renew the Tier 1 permit for this facility. Per the guidance listed in IDAPA 58.01.01.313.03 of Idaho Rules for the Control of Air Pollution, Sinclair is submitting this application nine months prior to operating permit expiration.

Sinclair is also currently operating under the provisions of its Tier 2 operating permit as revised on August 20, 2003. The current Tier 2 permit expires on October 30, 2007. Because of the similarity between the provisions of the Tier 1 and Tier 2 permits, Sinclair is requesting this Tier 1 permit application renewal also be used as the Tier 2 permit application renewal. By combining the Tier 1 and Tier 2 applications in this manner, Sinclair believes there with be considerable savings on the time and effort both the Division and Sinclair will spend processing these documents.

In compiling this operating permit application renewal, Sinclair is using the same format used for previous operating permit applications. Sinclair believes this format is acceptable to the Division and complies with the requirements of IDAPA 58.01.01.314 of Idaho Rules for the Control of Air Pollution.

Please note there are no substantial changes contained in this permit application, compared to the previous permit application, with exception of the addition of the Soil Vapor Extraction system. In general, Sinclair believes the provisions listed in the current Tier 1 and Tier 2 permits accurately reflect the applicable requirements for this facility.

Sinclair believes this operating permit application renewal is accurate, timely and complete and therefore requests the Division grant an operating permit application shield for both the Tier 1 and Tier 2 permits. Sinclair appreciates the assistance of the Division in facilitating these permit renewals. Should you have any questions regarding the information in this application, please call me at (801) 524-2729.

Respectfully,

Samuel B. Greene P.E.

Corporate Air Quality Engineer

attachments

CC:

M. Peterson w/o/a

J. Maffuccio w/o/a

D. Cole

TIER 1 OPERATING PERMIT APPLICATION - RENEWAL SINCLAIR BURLEY PRODUCTS TERMINAL SINCLAIR TRANSPORTATION COMPANY

Table of Contents

1.0	INTRODUCTION	E
2.0	PERMIT APPLICATION FORMS	6
3.0	GENERAL INFORMATION FOR THE FACILITY	7
4.0	EXCESS EMISSIONS PROCEDURES	9
5.0	EMISSIONS UNIT INFORMATION	10
6.0	INSIGNIFICANT ACTIVITIES	16
7.0	REGULATORY REQUIREMENTS	17
APF	PENDIX: A STORAGE TANK EMISSIONS CALCULATIONS	20
APF	PENDIX: B LOADING RACK EMISSIONS CALCULATIONS	21
APF	PENDIX: C FUGITIVE EMISSIONS CALCULATIONS	22
APF	PENDIX: D. PERMIT TO CONSTRUCT EXEMPTION - SVE	23

1.0 INTRODUCTION

Sinclair Burley Products Terminal, Sinclair Transportation Company (Sinclair) operates a petroleum products receipt, storage and distribution facility located in Burley, Idaho. This facility is currently operating under the provisions of Tier 1 Operating Permit No. T1-030413 and Tier 2 Operating Permit No. T2-030419. Tier 1 Operating Permit No. T1-030413 was issued on July 4, 2002 and revised on January 13, 2004. The current Tier 1 operating permit expires on July 4, 2007.

The Tier 2 operating permit was issued on October 30, 2002, revised on July 16, 2003 and revised again on August 20, 2003. The current Tier 2 operating permit expires on October 30, 2007.

Sinclair is requesting this Tier 1 permit application renewal also be used as the Tier 2 permit application renewal. By combining the Tier 1 and Tier 2 applications in this manner, Sinclair believes there with be considerable savings on the time and effort both the Division and Sinclair will spend processing these documents.

This permit application has been written to present all information required by the Division necessary to support a Tier 1 operating permit. The application is divided into the following chapters:

- Chapter 2.0: Contains the Tier 1 Operating Permit application forms required by DEQ.
- Chapter 3.0: Contains the general information for the facility.
- Chapter 4.0: Describes excess emissions procedures.
- Chapter 5.0: Provides information on emissions units.
- Chapter 6.0 Lists insignificant activities.
- Chapter 7.0: Addresses the regulatory requirements for this facility.
- Chapter 8.0: Contains the compliance certification.

2.0 PERMIT APPLICATION FORMS

The Tier 1 operating permit application forms for the Emissions Units (EU) listed in Table 2.1 are presented in this chapter.

Table 2.1 Listing of Emissions Units

EU#	Description Description
1	Tank 301
2	Tank 304
3	Tank 311
4	Tank 321
5	Tank 302
6	Tank 305
7	Tank 306
8	Transmix Tank
9	Prover Tank
10	Loading Rack
11	Fugitive Emissions
N/A	Soil Vapor Extraction System

SECTION 1: GENERAL INFORMATION

COMPANY & DIVISION NAME	SINCLAIR BI	URLEY PRO	DUCTS TERMIN	AL, SINCLAIR	TRANSPORTATION CO	MPANY Tier 1/Tier 2	2 Renewal, 10/9/06	***************************************
STREET ADDRESS OR P.O. BOX	425 East High	hway 81			kaja ja ja art 1900 kilonen popuja ja ja arana, popuje kilonen restriki keleksi kanada kaja asa Kilonen ja	immetati yana yana ayan ayan ayan ayan ayan aya		
CITY	Burley							
STATE (ID	ZIP	83318						
PERSON TO CONTACT	Facility Conta	ct: Dave Col	le / Permitting C	Contact: Samue	el B. Greene P.E.			
TITLE (1987 - 1987)	Terminal Man	nager	/ Corporate	Air Quality Engi	neer			
PHONE NUMBER	(208) 678-7	7363	(801) 524-	2729]			
EXACT PLANT LOCATION	T-10, S-36, R	-23E						
GENERAL NATURE OF BUSINESS	Petroleum pro	oducts receipt	t, storage and di	stribution				
NUMBER OF FULL-TIME EMPLOYEES	2							
PROPERTY AREA (ACRES)	Арргох. 15				REASON FOR APPLIC (1) Permit to Construct (2) Permit to Modify an (3) Permit to Construct (4) Change of Owner of (5) Tier I Permit to Ope (6) Tier II Permit to Op (7) Tier II Permit to Ope	t a new facility; n existing source; t a new source at an or or Location; erate; erate		
DISTANCE TO NEAREST STATE BORDE	R (MILES)		30					
PRIMARY SIC	5171]			SECONDARY SIC		5171	
PLANT LOCATION COUNTY	Cassia]			ELEVATION (FT)		4180	
UTM ZONE	72							
UTM (X) COORDINATE (KM)	277123				UTM (Y) COORDINATE	(KM)	4710315	
NAME OF FACILITIES List all facilities within the state that are und	er your control,		OF OTHER FAC		ns to the air. If none, so s	tate		
Burley Products Terminal]	425 East Hv	vy. 81 Burley, IC	9 83318 Cass	ia County			
Boise Products Terminal]	712 North C	urtis Boise, ID	83706 Ada Co	unty			
	J		et periodici in territorio de la companio de la co La companio de la co		aj angraja, maken eren eren eren induka kan da paja, aj en eren eren eren eren kan araban kan da era kan da a Maken eren eren eren eren eren eren eren e			
	J				ian appening period to the territories and the second security of the second second second second second second The second s			
]							
OWNER OR RESPONSIBLE OFFICIAL		Mark Peters	en					
TITLE OF RESPONSIBLE OFFICIAL		Vice Preside	ent, Sinclair Tran	sportation Com	pany			
Based on information and belief formed afte document are true, accurate, and complete.		quiry, I certify	the statements	and information	in this			
SIGNATURE OF OWNER OR RESPONSI	3LE OFFICIAL	injunacione de la company		parties are accessed as a success of the least of the parties of the least of the l	enschausengewarten der Anderson der seiner gerichte gestellt und der Stelle der Gregorie	DATE		
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SECTION 3: PROCESS AND MANUFACTURING OPERATIONS

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DEQ PLANT ID CODE		DEQ PROCESS COD		DEQ STACK ID CODE		
DEQ BUILDING ID CODE		PRIMARY SCC		SECONDARY SCC		
DEQ SEGMENT CODE						
PART A: GENERAL I	NFORMATION	териверия неневрения переих это не почето по почето по почето почето почето почето почето почето почето почет Почето почето почет	такжа и компроизвения выпораторующих порт сточения под под подажения выпораторующих под под под под под под под		ов в достигно в в в в в в в в в в в в в в в в в в в	universität valka ja kan kan kan kan kan kan kan kan kan ka
PROCESS CODE OR DES	SCRIPTION	EU#1 (TK #301), EU#	2 (TK #304), EU#3 (TK #31	1), EU#4 (TK #321) Tier 1	/Tier 2 Renewal, 10/9/06	
STACK DESCRIPTION		N/A		et an arang an arang An arang an		
BUILDING DESCRIPTION		NA				
MANUFACTURER	N/A		MODEL	Ext. Floating Roof	DATE INSTALLED OR	1950
PROCESSII	NG DATA				but Your to 1993 out 17 1 has but	
PROCESS STREAM	MATERIAL DESCRIPTION	MAXIMUM HOURLY RATE	ACTUAL HOURLY RATE	ACTUAL ANNUAL RATE	UNITS	
INPUT	Gasoline	65,100			gal	
PRODUCT OUTPUT	Gasoline	65,100			gal	
WASTE OUTPUT						
RECYCLE						
POTENTIAL	HAPS IN PROCESSING STRE	AMS				
PS DESCRIPTION		HAP CAS NUMBER	FRACTION IN INPUT STREAM BY WEIGHT	FRACTION IN PRODUCT STREAM BY WEIGHT	FRACTION IN WASTE STREAM BY WEIGHT	FRACTION IN F
Benzene		71-43-2	004250	004250		
Hexane		110-54-3	00350	00350		
Xylenes (mixed isomers)		1330-20-7	01777	01777		
Toluene		108-88-3	02180	02180		
Ethylbenzene		100-41-4	002860	002860		
Naphthalene		91-20-3	00064	00064		
Trimethylpentane (2,2,4)		540-84-1	008432	008432		

0-.0025

0-.0025

98-82-8

SECTION 5: STORAGE AND HANDLING OF LIQUID SOLVENTS & OTHER VOLATILE COMPOUNDS

DEQ USE ONLY	annan copilità de mandre en mante en constante de la company de la compa	TO NOT THE OWNER, WAS ARREST AND THE OWNER,				
DEQ PLANT ID CODE	DEQ PROCESS CODE			DEQ STACK ID COD	35	
DEQ BUILDING ID CODE	PRIMARY SCC			SECONDARY SCC		
DEQ SEGMENT CODE		ти в видели в под			grandersteller am Frenge und ausgebrucken eine Abbertreiten an der eine eine Abbertreiten für der eine eine ge	
	о физумация, него постоя на положно и наружения учера для тей постоя него положения положения по постоя на пост		era de prima sen consecuença de que de prima de definida de la consecuencia de prima de la consecuencia de prima de la consecuencia del la consecuencia de la consecuencia della consecuencia della della consecuencia della c			
PARIA: GENERAL INFORMATION					art atquis aus area	
PROCESS CODE OR DESCRIPTION	EU#1 (TK #301), EU#2 (TK	(#304), EU#3 (TK	#311), EU#4 (TK #321)	Tier 1/Tier 2 Renew	val, 10/9/06	
STACK DESCRIPTION	N/A					
BUILDING DESCRIPTION	N/A		matroson do duniya wanaya wa againin indoniya haya karaya kanada wa wa wa wa wa ka da ka ka ka ka ka ka ka ka k			
DATE INSTALLED OR 1950 LAST MODIFIED						
GENERAL TANK AND MATERIAL HANDLI	NG DATA					
MATERIAL DESCRIPTION Gasoline						
TANK CAPACITY (GALLONS) 840,000	ANNUAL THROUGHPUT (GALLONS)	86.359 E 6]		
TANK TYPE 2		SOURCE]		
PLEASE CHOOSE FROM BELOW (01) FIXED ROOF:		PLEASE CHOO (01) PIPELINE	SE FROM BELOW			
(02) FLOATING ROOF (OR INTERNAL COVER);		(02) RAIL CAP	₹;			
(03) VARIABLE VAPOR SPACE; (04) PRESSURE TANK;		(03) TANK TR (04) SHIP BAF		:		
(05) UNDERGROUND - SPLASH LOADING:	and an analysis and a reconstruction of the second and the second and the second and the second and the second	(05) OTHER				
(06) OTHER						
ADDITIONAL VAPOR PHASE DEGREASING	2 DATA	····			r	
MANUFACTURER OF DEGREASING AGENT N/A	apara paga ay tanining mang pangkalanda ay ana a	***************************************		TANK SURFACE ARI	ĒA (SQ. FT)	e Tanks 4.0
TEMPERATURE OF DEGREASING AGENT IN TANK (DEG	i, F)	N/A		METHOD OF VAPOR	RECOVERY	6
				Please choose from b (01) Incineration;		
				(02) Refrigerated Lic (03) Refrigerated Co	ondenser,	
				(04) Carbon Adsorp (05) Vapor Return S	System;	
				(06) No Recovery S (07) Other	VSIBIN.	
				(as) On the passessessesses		
ADDITIONAL MATERIAL HANDLING DATA						
PHYSICAL STATE	NUMBER OF		NUMBER OF COMPRE	Engage and a second	NUMBER OF IN-LINE	
(SEE NOTE BELOW)	PUMP SEALS	0]	SEALS	Lol	VALVES	11
NUMBER OF SAFETY	NUMBER OF	20	NUMBER OF OPEN-E	NDED 0	NUMBER OF SAMPLING CONNECTIONS	6
RELIEF VALVES 1	FLANGES	201	LINES	<u> </u>	COMMECTIONS L	manage of a
MATERIAL DATA						
HAP DESCRIPTION	HAP CAS		НА	AP FRACTION IN		
Benzene	NUMBER 71-43-2]	MAT	ERIAL BY WEIGHT		
Hexane	110-54-3			0-0350		
Xylenes (mixed isomers)	1330-20-7]		0-1777		
Toluene	108-88-3]		0-2180		
Ethylbenzene	100-41-4]	m.	002860		
Naphthalene	91-20-3]		00064		
Trimethylpentane (2,2,4)	540-84-1]	. 30	008432		
opropyi Benzene	98-82-8]	{	0-,0025		

NOTE: PHYSICAL STATE - V) VAPOR LIGHT; L) LIQUID LIGHT; H) HEAVY LIGHT

SECTION 5, PART B	U#1 (TK #301), EU#2 (TK #304), EU#3 (TK #311), EU#4 (TK #321)	Tier 1/Tier 2 Renewal, 10/9/	26					
OPERATING DATA PERCENT FUEL CONSUMPTION PER QUARTER		OPERATING SCHEDULE							
DEC-FEB 25		HOURS/DAY	24						
MAR-MAY 25		DAYS/WEEK	7						
JUN-AUG 25		WEEKS/YEAR	52						
SEP-NOV 25									
PARAMETER PARAMETER	PRIMARY		SECONDAR'	Y					
TYPE	N/A horizontal professional construction and construction		N/A and an analysis of the second						
TYPE CODE (FROM APP. A)									
MANUFACTURER									
MODEL NUMBER		British or Bertin Advice than the control of the co	gad fallen til finde state sta						
PRESSURE DROP (IN. OF WATER)]					
WET SCRUBBER FLOW (GPM)									
BAGHOUSE AIR/CLOTH RATIO (FPM)									
VENTILATION AND BUILD	ING/AREA DATA	STACK DAT	A						
ENCLOSED? (Y/N)		GROUND ELEVATION (FT)	ı		N/A				
HOOD TYPE (FROM APP. B)		UTM X COORDINATE (KM)							
MINIMUM FLOW (ACFM)		UTM Y COORDINATE (KM)							
PERCENT CAPTURE EFFICIENCY		STACK TYPE (SEE NOTE BELOW)							
BUILDING HEIGHT (FT)		STACK EXIT HEIGHT FROM GROUND LEVEL (FT)							
BUILDING LENGTH (FT)		STACK EXIT DIAMETER (F	T)						
BUILDING WIDTH (FT)		STACK EXIT GAS FLOWRA	ATE (ACFM)						
		STACK EXIT TEMPERATUR	RE (DEG. F)						
AIR POLLUTANT EMISSIO	NS								
POLLUTANT CAS NUMBER	EMISSION FACTOR	PERCENT CONTROL	ESTIMATED OR MEASURED	ALLOWA	BLE EMISSIONS	3			
	(SEE NOTE BELOW)	EFFICIENCY	EMISSIONS (LBS/HR)	(LBS/HR)	(TONS/YR)	REFERENCE			
PM									
PM-10									
SO2									
со			And the state of t						
NOx									
VOC	Tanks 4.0	0	3.46	3.46	15,17	Tanks 4.0			
LEAD		frames and an experimental properties of the second of the	franconneus anno esta de disconneus consecutarios personal properto de la consecutario de						
Benzene 71-43-2	Tanks 4.0	o	1.887E-02	1.887E-02	8.266E-02	Tanks 4.0			
Hexane 110-54-3	Tanks 4.0	0	3.002E-02	3.002E-02	1.315E-01	Tanks 4.0			
Xylenes (mixed isomers) 1330-20-7	Tanks 4.0	0	1.158E-02	1.155E-02	5.059E-02	Tanks 4.0			
Toluene 108-88-3	Tanks 4.0	0	2.866E-02	2.866E-02	1.255E-01	Tanks 4.0			
Ethylbenzene 100-41-4	Tanks 4.0	o	2.358E-03	2.358E-03	1.033E-02	Tanks 4.0			
Naphthalene 91-20-3	Tanks 4.0	0	4.224E-05	4.224E-05	1.850E-04	Tanks 4.0			
Trimethylpentane (2,2,4) 540-84-1	Tanks 4.0	O mingralizationarea universal anhazanario coupragendo pulsa envelope in constructivo constructivo de la constructivo de pulsa envelope in constructivo constructivo de la constructivo	7.862E-03	7.862E-03	3.444E-02	Tanks 4.0			
isopropyi Benzene 98-82-8	Tanks 4.0	0	1.518E-04	1.518E-04	6.650E-04	Tanks 4.0			
The second secon				" i se salainis ainminante	The second secon				

STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

NOTES:

SECTION 3: PROCESS AND MANUFACTURING OPERATIONS

Naphthalene

DEQ USE ONLY		interpretation of the state of	and production and the compression of the compressi	nkain salaman 1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (1970 (Only Computer our Participation of Control of Management of Space (Print Management our company of Space (Space	
DEQ PLANT ID CODE		DEQ PROCESS COL	DE []	DEQ STACK ID CODE		
BUILDING ID CODE		PRIMARY SCC		SECONDARY SCC		
DEQ SEGMENT CODE						
PART A: GENERALIN	FORMATION		дер (Монте в Ангрия) по постоя на постоя	an managan man Pangan managan	da Maramening et allektronie in inventering gaza zapit 1649 dari cala interferencia program.	
PROCESS CODE OR DESC	CRIPTION	EU#5 (TK #302), EU#	/6 (TK #305), EU#7 (TK #30	06) Tier 1/Tier 2 Renewal,	10/9/06	
STACK DESCRIPTION						
BUILDING DESCRIPTION		N/A		n para kanangan pengahan dan kananan kanangan pengahan dan kanangan pengahan pengahan kanangan pengahan berana Kanangan pengahan dan kanangan pengahan kanangan pengahan kanangan kanangan pengahan pengahan kanangan pengaha		
MANUFACTURER		nd fan de specier verse en een staat de de ferste fende fende de fende de fende de specier en een een de fende de se Tot de specier en een een een een een een een een ee	MODEL	Cone Roof	DATE INSTALLED OF	1950
PROCESSIN	G DATA					
PROCESS STREAM	MATERIAL DESCRIPTION	MAXIMUM HOURLY RATE	ACTUAL HOURLY RATE	ACTUAL ANNUAL RATE	UNITS	
INPUT	Distillate Fuel Oil	58,800			gal	
PRODUCT OUTPUT	Distillate Fuel Oil	58,800			gal	
WASTE OUTPUT						
RECYCLE						
POTENTIAL	HAPS IN PROCESSING STR	EAMS				
SCRIPTION		HAP CAS NUMBER	FRACTION IN INPUT STREAM BY WEIGHT	FRACTION IN PRODUCT STREAM BY WEIGHT	FRACTION IN WASTE STREAM BY WEIGHT	FRACTION IN RECYCLE STREAM BY WEIGHT
Benzene		71-43-2	000003	000003		
Xylenes (mixed isomers)		1330-20-7	000082	000082		
Toluene		108-88-3	000019	000019		

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0-,00170

SECTION 5: STORAGE AND HANDLING OF LIQUID SOLVENTS & OTHER VOLATILE COMPOUNDS

DEQ USE ONLY	edekalarini riccio (n. 1. maggazia) deserva maggazia per esca spilo escoco e má de la compresso por porte esco					
DEQ PLANT ID CODE	DEQ PROCESS CODE			DEQ STACK ID CODE		
DEQ BUILDING ID CODE	PRIMARY SCC			SECONDARY SCC		1
DEQ SEGMENT CODE						
		erin 10 Ministerior (organization graduum matematempages)				
PARI A: GENERAL INFORMATION						
PROCESS CODE OR DESCRIPTION	EU#5 (TK #302), EU#6 (TR	(#305), EU#7 (TK	#306) Tier 1/Tier 2 F	Renewal, 10/9/06		
STACK DESCRIPTION	N/A]
BUILDING DESCRIPTION	N/A]
DATE INSTALLED OR 1950 LAST MODIFIED						
GENERAL TANK AND MATERIAL HANDLIN	IG DATA					
MATERIAL DESCRIPTION Distillate Fuel Oil						
TANK CAPACITY (GALLONS) 840,000	ANNUAL THROUGHPUT (GALLONS)	155.6 E 6]		
TANK TYPE 1 PLEASE CHOOSE FROM BELOW (01) FIXED ROOF; (02) FLOATING ROOF (OR INTERNAL COVER); (03) VARIABLE VAPOR SPACE; (04) PRESSURE TANK;		SOURCE PLEASE CHOO: (01) PIPELINE (02) RAIL CAR (03) TANK TRI (04) SHIP BAR	t; UCK;			
(05) UNDERGROUND - SPLASH LOADING;		(05) OTHER				Personal
(06) OTHER		(,	Special production consistency where the action and the action and the action and the action		(MITTERS AND AND AND AND AND AND AND AND AND AND	.i
	and the second desired and the second					
ADDITIONAL VAPOR PHASE DEGREASING	DATA					
MANUFACTURER OF DEGREASING AGENT N/A				TANK SURFACE AREA (S	Q. FT)	See Tanks 4.0
TEMPERATURE OF DEGREASING AGENT IN TANK (DEG	· F)	N/A		METHOD OF VAPOR REC Please choose from below: (01) Incineration; (02) Refrigerated Liquid S (03) Refrigerated Conden (04) Carbon Adsorption; (05) Vapor Return System (06) No Recovery System (07) Other	icrubber; iser; 1;	6
ADDITIONAL MATERIAL HANDLING DATA						
PHYSICAL STATE	NUMBER OF		NUMBER OF COMPRE	ESSOR	NUMBER OF IN-LINE	
(SEE NOTE BELOW)	PUMP SEALS	0	SEALS	0	VALVES	10
NUMBER OF SAFETY	NUMBER OF	-	NUMBER OF OPEN-E	NDED	NUMBER OF SAMPLI	νG
RELIEF VALVES 2	FLANGES	14	LINES	0	CONNECTIONS	4
MATERIAL DATA						
HAP DESCRIPTION	HAP CAS NUMBER			AP FRACTION IN ERIAL BY WEIGHT		
Benzene	71-43-2	J	inter i	000003		
Xylenes (mixed isomers)	1330-20-7]	and the second	000082		
Toluene	108-88-3			000019		
Naphthalene	91-20-3	1	1	000170		

NOTE: PHYSICAL STATE - V) VAPOR LIGHT; L) LIQUID LIGHT; H) HEAVY LIGHT

SECTION 5, PA	RT B	EU#5 (TK #302), EU#6 (TK	#305), EU#7 (TK #306) Tie	1/Tier 2 Renewal, 10/9/06			
PERCENT FUEL CON	OPERATING DATA SUMPTION PER QUARTER		OPERATING S	SCHEDULE	and management and an analysis		
DEC-FEB	25		HOURS/DAY	24			
MAR-MAY	28		DAYS/WEEK		1		
JUN-AUG	25		WEEKS/YEAR	52	i		
SEP-NOV	25			Material Conference of Conference on Confere	** -		
	POLLUTION CONTROL E	OUPMENT					
PARAMETER	in the State of th	PRIMARY			SECONDARY		
TYPE		N/A			The state of the s		
TYPE CODE (FROM A	PP. A)					<u>pariocolomora contrata con sincolomora de contrata de</u>	•
MANUFACTURER							
MODEL NUMBER							i e englis
PRESSURE DROP (IN.	OF WATER)]	· ·			
WET SCRUBBER FLO	W (GPM)			<i>*</i>			
BAGHOUSE AIR/CLOT	H RATIO (FPM)						
	VENTILATION AND BUILD	DING/AREA DATA	eal i te Magles	STACK DATA			
ENCLOSED? (Y/N)		N/A	GROUND ELEV	ATION (FT)		N/A	
HOOD TYPE (FROM A	PP. B)		UTM X COORD	INATE (KM)		Segretario de la constantina del constantina del constantina de la constantina de la constantina de la constantina de la constantina del constantina d	
MINIMUM FLOW (ACF	M):		UTM Y COORD	INATE (KM)		(many many many many many many many many	
PERCENT CAPTURE E	FFICIENCY		STACK TYPE (SEE NOTE BELOW)			
BUILDING HEIGHT (FT)		STACK EXIT H	EIGHT FROM GROUND LEV	/EL (FT)		
BUILDING LENGTH (FT	7		STACK EXIT DI	AMETER (FT)			
BUILDING WIDTH (FT)		per direktor kateria di kalendari di kalendari di kalendari di kalendari di kalendari di kalendari di kalendari Manta kalendari di kale	STACK EXIT G	AS FLOWRATE (ACFM)			
			STACK EXIT TE	EMPERATURE (DEG. F)			
/	AIR POLLUTANT EMISSIO	ons a la la maria de la					
POLLUTANT	CAS NUMBER	EMISSION	PERCENT	ESTIMATED OF	R ALLOW	ABLE EMISSIONS	3 .
		FACTOR (SEE NOTE	CONTROL EFFICIENCY	MEASURED EMISSIONS	(LBS/HR)	(TONS/YR)	REFERENCE
		BELOW)	for the second s	(LBS/HR)	**************************************	horizoniamistorniamistorniamist	-
PM							
PM-10				manipolarista formata de proposición de la compressión de la compressión de la compressión de la compressión d general polarisma de la compressión de			
SO2							
co							
NOx							
VOC		Tanks 4.0	O principal prin	0.09	0.09	0,39	Tanks 4.0
LEAD							
Benzene	71-43-2	Tanks 4.0		trivial	Purior State of State	trivial	Tanks 4.0
Xylenes (mixed isomers)	1330-20-7	Tanks 4.0		1.457E-03	1.457E-03	6.380E-03	Tanks 4.0
Toluene	108-88-3	Tanks 4.0	heary constructive and a solution of the solut	1.340E-03	1.340E-03	5.870E-03	Tanks 4.0
Nachthalene	91-20-3	Tanks 4.0	0	6 9636-05	8 9835.05	3.0505-04	Tanke 4 D

STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

NOTES:

SECTION 3: PROCESS AND MANUFACTURING OPERATIONS

DEQ USE ONLY					rannen a triling pending pending pending kenanta sebang kelakatah melang ana menungka	aderimentus en proponent protesta de la companya d
DEQ PLANT ID CODE		DEQ PROCESS CO	DE .	DEQ STACK ID CODE		
DEQ BUILDING ID CODE		PRIMARY SCC		SECONDARY SCC		
DEQ SEGMENT CODE						
PART A: GENERAL	INFORMATION	and the second s	у под при	en de financia de la composition della compositi		но Меженовый и не меженовый под
PROCESS CODE OR DES	SCRIPTION	EU#8, Transmix Tanl	k Tier 1/Tier 2 Renewal,	10/9/06		
STACK DESCRIPTION		N/A				
BUILDING DESCRIPTION		N/A				
MANUFACTURER	N/A		MODEL	Cone Roof	DATE INSTALLED OR LAST MODIFIED	1950
PROCESSI	NG DATA					
PROCESS STREAM	MATERIAL DESCRIPTION	MAXIMUM HOURLY RATE	ACTUAL HOURLY RATE	ACTUAL ANNUAL RATE	UNITS	
INPUT	Gasoline	65,100			gal	
PRODUCT OUTPUT	Gasoline	65,100			gal	
WASTE OUTPUT						
RECYCLE						
POTENTIA	_ HAPS IN PROCESSING STRI	EAMS				
2S DESCRIPTION		HAP CAS NUMBER	FRACTION IN INPUT STREAM BY WEIGHT	FRACTION IN PRODUCT STREAM BY WEIGHT	FRACTION IN WASTE STREAM BY WEIGHT	FRACTION IN F
Benzene		71-43-2	004250	004250		
Hexane		110-54-3	0- 0350	00350		
Xylenes (mixed isomers)		1330-20-7	01777	01777		
Toluene		108-88-3	02180	02180		
Ethylbenzene		100-41-4	002860	002860		
Naphthalene		91-20-3	00064	00064		
Trimethylpentane (2,2,4)	онного мень сенте в образова в обого в развите в образова в	540-84-1	0-08432	008432		
Isopropyl Benzene	nnanakanten inganisan nanjanannya panganannan terup. Dananning nyaman na inganisah pangangan panganan terup.	98-82-8	00025	00025		

SECTION 5: STORAGE AND HANDLING OF LIQUID SOLVENTS & OTHER VOLATILE COMPOUNDS

DEQ USE ONLY		Managaran da kanagaran da kanaga			
DEQ PLANT ID CODE	DEQ PROCESS CODE		DEQ STACK ID O	ODE	
DEQ BUILDING ID CODE	PRIMARY SCC		SECONDARY SC	c	***************************************
DEQ SEGMENT CODE					-
	tion copia kunik kita epakaria kita kekita unik kita edan juurun datus kankata kahit epita jaka ta kekita kata	a en anti-marchina de la companya d			
PAKI A: GENERAL INFORMATION					
PROCESS CODE OR DESCRIPTION		Tier 1/Tier 2 Renev	val. 10/9/06		outerus autoritas
STACK DESCRIPTION	N/A				and proving management
BUILDING DESCRIPTION	N/A				
DATE INSTALLED OR 1950 LAST MODIFIED					
GENERAL TANK AND MATERIAL HAND	DLING DATA				
MATERIAL DESCRIPTION Gasoline					•
TANK CAPACITY (GALLONS) 3,808	ANNUAL THROUGHPUT	(GALLONS)	38,080		
TANK TYPE 1		SOURCE			
PLEASE CHOOSE FROM BELOW (01) FIXED ROOF;		PLEASE CHOO: (01) PIPELINE	SE FROM BELOW		
(02) FLOATING ROOF (OR INTERNAL COVER); (03) VARIABLE VAPOR SPACE;		(02) RAIL CAR (03) TANK TRI	•		
(04) PRESSURE TANK;		(04) SHIP BAR		et Geologia kalandari da salang da samung kanang kaphana may kabada kalandari da Sami di Safara magi	minump
(05) UNDERGROUND - SPLASH LOADING;	necessaries de la companya de la com	(05) OTHER	Facility sump, vaccum truck		
(06) OTHER					
ADDITIONAL VAPOR PHASE DEGREAS	ING DATA				
MANUFACTURER OF DEGREASING AGENT N/A			TANK SURFACE	AREA (SQ. FT)	See Tanks 4.0
TEMPERATURE OF DEGREASING AGENT IN TANK (D	eg Fl	[N/A	METHOD OF VAP	OR RECOVERY	6
		Commence	Please choose from (01) Incineration;	n below:	-
			(02) Refrigerated (03) Refrigerated	Liquid Scrubber;	
			(04) Carbon Ads (05) Vapor Retur	orption; n System;	
			(06) No Recover	/ System;	
			(Or) Calest	Менаминий принути прин	atamining construction and an artist of the second
ADDITIONAL MATERIAL HANDLING DA	•				
PHYSICAL STATE (SEE NOTE BELOW)	NUMBER OF PUMP SEALS	0	NUMBER OF COMPRESSOR SEALS 0	NUMBER OF IN-LII VALVES	NE 2
NUMBER OF SAFETY	NUMBER OF		NUMBER OF OPEN-ENDED	NUMBER OF SAMI	hammananananani
RELIEF VALVES 0	FLANGES	4	LINES 0	CONNECTIONS	2
			. Annihome for Annihologic Ann		Annual department of the factor of the facto
MATERIAL DATA					
HAP DESCRIPTION	HAP CAS NUMBER		HAP FRACTION IN MATERIAL BY WEIGHT		
Benzene	71-43-2		0-04250		
Hexane	110-54-3		00350		
Xylenes (mixed isomers)	1330-20-7		Constitution of the second of		
Taluene	108-88-3		0-2180		
Ethylbenzene	100-41-4]	002880		
Naphthalene	91-20-3		00064		
Trimethylpentane (2,2,4)	puside minimum market m		008432		
sopropyl Benzene	98-82-8	1	0-0025		
manufacturing and the same of	C-02-0	-4			

NOTE: PHYSICAL STATE - V) VAPOR LIGHT; L) LIQUID LIGHT; H) HEAVY LIGHT

SECTION 5, PART B	U#8, Transmix Tank Tier 1/Tier 2 Re	newal, 10/9/06		2.4		
OPERATING DATA			ana ja nora-ju (akkonin jain ja			
PERCENT FUEL CONSUMPTION PER QUARTER		OPERATING SCHEDULE				
DEC-FEB 25		HOURS/DAY	24			
MAR-MAY 25		DAYS/WEEK	7]			
JUN-AUG 25		WEEKSMEAR	52			
SEP-NOV 25						
POLLUTION CONTROL EC	QUIPMENT					
PARAMETER	PRIMARY		SECONDAF	RY		
TYPE	NA		N/A			
TYPE CODE (FROM APP. A)				mound		
MANUFACTURER						
MODEL NUMBER						
PRESSURE DROP (IN. OF WATER)				1		
WET SCRUBBER FLOW (GPM)	printerportion on the contract and printerportion of the contract of the contr					
BAGHOUSE AIR/CLOTH RATIO (FPM)				<u> </u>		
VENTILATION AND BUILD	HNG/AREA DATA	STACK DAI	ra.			
ENCLOSED? (Y/N)	N/A	GROUND ELEVATION (FT			N/A	
HOOD TYPE (FROM APP. B)		UTM X COORDINATE (KM	<i>*</i>		1	
MINIMUM FLOW (ACFM)		UTM Y COORDINATE (KM				
PERCENT CAPTURE EFFICIENCY	All the beautiful resident and an interpretation parameters represented by a contract of the c	STACK TYPE (SEE NOTE			The state of the s	
BUILDING HEIGHT (FT)	descriptions of the control of the c	STACK EXIT HEIGHT FRO				
BUILDING LENGTH (FT)	emonoment proton and an activation and produce and activation activation activation and activation activ	STACK EXIT DIAMETER (F				
BUILDING WIDTH (FT)	Commence and company in commence and commenc	STACK EXIT GAS FLOWR	ATE (ACFM)			
	securios escas antidos de infesta de solido de contrator	STACK EXIT TEMPERATU	RE (DEG. F)			

POLLUTANT CAS NUMBER	NS EMISSION	PERCENT	ESTIMATED OR	ALI OWA	BLE EMISSIONS	Tesa I
	FACTOR (SEE NOTE BELOW)	CONTROL EFFICIENCY	MEASURED EMISSIONS (LBS/HR)	(LBS/HR)	(TONS/YR)	REFERENCE
PM Section 1						
PM-10	Security of the Conference of	the transfer the second of the				
SO2	Neutran de la socia de la montación con escucion misera insularia de la montación de grada de la misera del del montación de la montación de la montación del porte de la montación de la mon				Longer Commence Comme	
co	frame construction of the		And a second contract of the second contract	· Professional Control	. Increase and the second	Contraction of the contraction o
NOx	and the state of t		no manufactura para na procesa na manda procesa na managa na managa na managa na managa na managa na managa na Procesa na managa na			***************************************
VOC	Tanks 4.0		0.06	0.06	0.27	Tanks 4.0
LEAD	This bid opposite interest control for an annual control contr					
Benzene 71-43-2	Tanks 4.0	0	3.345E-04	3.345E-04	1.465E-03	Tanks 4.0
Hexane 110-54-3	Tanks 4,0	0	5.388E-04	5.388E-04	2.360E-03	Tanks 4.0
Xylenes (mixed isomers) 1330-20-7	Tanks 4.0	O	1.404E-04	1.404E-04	6.150E-04	Tanks 4.0
Toluene 108-88-3	Tanks 4.0	0	4.692E-04	4.692E-04	2.055E-03	Tanks 4.0
Ethylbenzene 100-41-4	Tanks 4.0	0	3.082E-05	3.082E-05	1.350E-04	Tanks 4.0
Naphthalene 91-20-3	Tanks 4.0	0	trivial	trivial	trivial	Tanks 4.0
Trimethylpentane (2,2,4) 540-84-1	Tanks 4.0		1.347E-04	1.347E-04	5.900E-04	Tanks 4.0
Isopropyi Benzene 98-82-8	Tanks 4.0		1.142E-06	1.142E-06	5.000E-06	Tanks 4.0

NOTES: STACK TYPE - 01) DOWNWARD, 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

SECTION 3: PROCESS AND MANUFACTURING OPERATIONS

DEQ USE ONLY	An tide control of the control of th	and an earth place in the Colonia from the colonia for the colonia for the colonia colonia for the colonia for				
DEQ PLANT ID CODE		DEQ PROCESS COD		DEQ STACK ID CODE		
BUILDING ID CODE		PRIMARY SCC		SECONDARY SCC		
DEQ SEGMENT CODE					and by althous was a few amount demonstratives or few are serious and serious	
PART A: GENERAL	INFORMATION					
PROCESS CODE OR DES	SCRIPTION	EU#9 , Prover Tank	Tier 1/Tier 2 Renewal, 1	0/9/06		
STACK DESCRIPTION		N/A				
BUILDING DESCRIPTION		N/A				
MANUFACTURER	N/A		MODEL	Cone Roof	DATE INSTALLED OR	1950
PROCESSI	NG DATA				LAST MODIFIED	
PROCESS STREAM	MATERIAL DESCRIPTION	MAXIMUM HOURLY RATE	ACTUAL HOURLY RATE	ACTUAL ANNUAL RATE	UNITS	
INPUT	Gasoline	65,100				
PRODUCT OUTPUT	Gasoline	65,100			gal	
WASTE OUTPUT						
RECYCLE						
POTENTIAL	. HAPS IN PROCESSING STR	REAMS				
SCRIPTION		HAP CAS NUMBER	FRACTION IN INPUT STREAM BY WEIGHT	FRACTION IN PRODUCT STREAM BY WEIGHT	FRACTION IN WASTE STREAM BY WEIGHT	FRACTION IN RECYCLE STREAM BY WEIGHT
Benzene		71-43-2	004250	004250		
Hexane		110-54-3	00350	00350		
Xylenes (mixed isomers)		1330-20-7	0-,1777	01777		
Toluene		108-88-3	02180	02180		
Ethylbenzene		100-41-4	002860	0- 02860		
Naphthalene		91-20-3	00064	00064		
Trimethylpentane (2,2,4)		540-84-1	0-08432	008432		
Isopropyl Benzene		98-82-8	00025	00025		

SECTION 5: STORAGE AND HANDLING OF LIQUID SOLVENTS & OTHER VOLATILE COMPOUNDS

DEQ USE ONLY		lin territorio monte de la composito de la comp					
DEQ PLANT ID CODE		DEQ PROCESS CODE			DEQ STACK ID CODE		
DEQ BUILDING ID CODE		PRIMARY SCC			SECONDARY SCC		
DEQ SEGMENT CODE							
PARIA: GENERALINE	ORMATION		oorwoonse noorween standard on the contract of	адистопуской болов на надачения по продости по не на продости на продости на продости на подости на подости на На применения на применения на продости на продости на продости на продости на продости на продости на продост	rintratinia il reconsidenti (en manuscuscuscuscuscuscuscuscus) di septimizza reprosedu provincia para coggi popu	TO COMPANY TO THE PROPERTY OF	невич и селото розпочение по во пред селото по выпоснова на пред на под поставления до поставления до поставле
PROCESS CODE OR DESCR	RIPTION	EU#9 , Prover Tank Ti	er 1/Tier 2 Renewa	al, 10/9/06			1
STACK DESCRIPTION		N/A					
BUILDING DESCRIPTION		N/A					
DATE INSTALLED OR LAST MODIFIED	1950						
GENERAL TAN	IK AND MATERIAL HANDLI	NG DATA					
MATERIAL DESCRIPTION	Gasoline						
TANK CAPACITY (GALLONS)	735	ANNUAL THROUGHPUT	(GALLONS)	220,220			
TANK TYPE	1		SOURCE	5			
PLEASE CHOOSE FROM BE (01) FIXED ROOF; (02) FLOATING ROOF (OR	7.12		(01) PIPELINE				
(03) VARIABLE VAPOR SPA			(02) RAIL CAF (03) TANK TR	UCK;			
(04) PRESSURE TANK; (05) UNDERGROUND - SPE	ASH LOADING:		(04) SHIP BAR (05) OTHER	RGE; Facility tank farm			7
(06) OTHER			, , , , , , , , , , , , , , , , , , , ,	Annual protection of the contraction of the contrac	n (1941) in the state of the st	artical (Color Color Col	
ADDITIONAL V	APOR PHASE DEGREASING	G DATA					
MANUFACTURER OF DEGRE	EASING AGENT N/A				TANK SURFACE AREA (SC	2. FT)	See Tanks 4.0
TEMPERATURE OF DEGREA	SING AGENT IN TANK (DEG	(F)	N/A		METHOD OF VAPOR RECO	OVERY	6
					Please choose from below: (01) Incineration; (02) Refrigerated Liquid Si	crubber:	
					(03) Refrigerated Condens(04) Carbon Adsorption;	ser;	
					(05) Vapor Return System (06) No Recovery System		***************************************
					(07) Other		
ADDITIONAL M PHYSICAL STATE	ATERIAL HANDLING DATA	ibaa a-					
(SEE NOTE BELOW)	F	NUMBER OF PUMP SEALS	0	NUMBER OF COMPRE	SSOR	NUMBER OF IN-LINE VALVES	2
NUMBER OF SAFETY		NUMBER OF		NUMBER OF OPEN-EN	IDED	NUMBER OF SAMPLI	procession and a second
RELIEF VALVES	0	FLANGES	6	LINES		CONNECTIONS	0
MATERIAL DAT	<u>.</u>						
HAP DESCRIPTION		HAP CAS NUMBER		HAI MATE	P FRACTION IN RIAL BY WEIGHT		
Benzene		71-43-2			004250		
Hexane		110-54-3			00350		
Xylenes (mixed isomers)		1330-20-7			0-, 1777		
Toluene		108-88-3			02180		
Ethylbenzene		100-41-4		la co	002860		
Naphthalene		91-20-3]	au de la company	0-0064		
Trimethylpentane (2,2,4)		540-84-1]		008432		
Isopropyl Benzene	Marie Marie Committee Anna Caracter Strategies Services S	98-82-8]	Γ	00025		

NOTE: PHYSICAL STATE - V) VAPOR LIGHT; L) LIQUID LIGHT; H) HEAVY LIGHT

SECTION 5, PART B	EU#9 , Prover Tank Tier 1/Tier 2 Ren	ewal, 10/9/06	
OPERATING DATA			·
PERCENT FUEL CONSUMPTION PER QUARTI	ER 	OPERATING SCHEDULE	
DEC-FEB	25	HOURS/DAY 24	
MAR-MAY 2	25	DAYS/WEEK 7	
JUN-AUG 2	25	WEEKS/YEAR 52	
SEP-NOV 2	25		
POLLUTION CONTRO	L EQUIPMENT		
PARAMETER	PRIMARY	SECONDAR	Y
TYPE	LNA	N/A	
TYPE CODE (FROM APP. A)		AND	A THE COLUMN TWO IS NOT THE COLUMN TWO IS NO
MANUFACTURER	Records of Contract C		
MODEL NUMBER		- International Control of the Contr	
PRESSURE DROP (IN. OF WATER)			
WET SCRUBBER FLOW (GPM)			
BAGHOUSE AIR/CLOTH RATIO (FPM)	homosomonomonia.		
VENTILATION AND BU	UILDING/AREA DATA	STACK DATA	general responsibility of the second
ENCLOSED? (Y/N)	N/A protection and a second and	GROUND ELEVATION (FT)	N/A
HOOD TYPE (FROM APP. B)		UTM X COORDINATE (KM)	
MINIMUM FLOW (ACFM)		UTM Y COORDINATE (KM)	
PERCENT CAPTURE EFFICIENCY		STACK TYPE (SEE NOTE BELOW)	Parameter of the control of the cont
BUILDING HEIGHT (FT)		STACK EXIT HEIGHT FROM GROUND LEVEL (FT)	and the second s
BUILDING LENGTH (FT)		STACK EXIT DIAMETER (FT)	
BUILDING WIDTH (FT)		STACK EXIT GAS FLOWRATE (ACFM)	
		STACK EXIT TEMPERATURE (DEG. F)	
AIR POLLUTANT EMIS	SIONS		
POLLUTANT CAS NUMBER	EMISSION FACTOR	PERCENT ESTIMATED OR CONTROL MEASURED	ALLOWABLE EMISSIONS
	(SEE NOTE BELOW)	EFFICIENCY EMISSIONS (LBS/HR)	(LBS/HR) (TONS/YR) REFERENCE
PM			
PM-10			
SO2			
СО			
NOx			
voc	Tanks 4.0	0 0.06	0.06 0.26 Tanks 4.0
LEAD			
Benzene 71-43-2	Tanks 4.0	0 3.139E-04	3.139E-04 1.375E-03 Tanks 4.0
Hexane 110-54-3	Tanks 4.0	0 5.057E-04	5.057E-04 2.215E-03 Tanks 4.0
Xylenes (mixed isomers) 1330-20-7	Tanks 4.0	0 1.313E-04	1.313E-04 5.750E-04 Tanks 4.0
Toluene 108-88-3	Tanks 4.0	0 4.406E-04	4.406E-04 1.930E-03 Tanks 4.0
Ethylbenzene 100-41-4	Tanks 4.0	0 2.968E-05	2.968E-05 1.300E-04 Tanks 4.0
Naphthalene 91-20-3	Tanks 4.0	O (trivial	trivial trivial Tanks 4.0
Trimethylpentane (2,2,4) 540-84-1	Tanks 4.0	0 1.267E-04	1.267E-04 5.550E-04 Tanks 4.0
Isopropyl Benzene 98-82-8	Tanks 4.0	0 1.142E-06	1.142E-06 5.000E-06 Tanks 4.0

NOTES: STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

SECTION 6: LOADING RACKS

DEQ USE ONLY		
DEQ PLANT ID CODE	DEQ PROCESS CODE DEQ STACK ID CODE	nonconne
DEQ BUILDING ID CODE	PRIMARY SCC SECONDARY SCC	The second second
DEQ SEGMENT CODE		
PART A: LOADING RACK DATA		од о основного в горија о од основного од обого од основного основного од основного
PROCESS CODE OR DESCRIPTION	EU#10 , GASOLINE LOADING Tier 1/Tier 2 Renewal, 10/9/06	opening to the state of the sta
STACK DESCRIPTION	N/A	
BUILDING DESCRIPTION	N/A	nous seepe
MANUFACTURER N/A	MODEL N/A DATE INSTALLED LAST MODIFIED	OR 1950*
TYPE OF LOADING	Bottom Loading	
LOADING ARM VAPOR ENCLOSURE	None - open to air, dry brake coupler	
MATERIAL LOADED	Gasoline	
ANNUAL THROUGHPUT (gallons)	107.310 E 6	
True Vapor Pressure (psia), annual average	4.1037	
MAX. TEMP (F)	54	
AVG. TEMP (F)	46	

^{*} The loading rack was converted from top loading to bottom loading in 1994-1995.
See August 3, 2000 correspondence from Sinclair to Mr. D. E. Hardesty, USEPA region 8

SECTION 6, PART B	EU#10 , GASOLINE LOADING	Tier 1/Tier 2 Renewal, 10/9/06	
OPERATING DATA PERCENT FUEL CONSUMPTION PER QUARTE	:	OPERATING SCHEDULE	
	· Barrio Antonia	- Control of the Cont	
Parameter in programment in the control of the cont	7	HOURS/DAY 24	
MAR-MAY 2:	<u> </u>	DAYS/WEEK 7	
JUN-AUG 26	7	WEEKS/YEAR 52	
SEP-NOV 20	***************************************		
POLLUTION CONTROL PARAMETER	LEQUIPMENT PRIMARY	SI	gadija — Byayar III a d ECONDARY
TYPE	N/A		
TYPE CODE (FROM APP. A)	parameteria de la constitución d		
MANUFACTURER			
MODEL NUMBER			
PRESSURE DROP (IN. OF WATER)			
WET SCRUBBER FLOW (GPM)			
BAGHOUSE AIR/CLOTH RATIO (FPM)			
VENTILATION AND BU	ILDING/AREA DATA	STACK DATA	
ENCLOSED? (Y/N)	N/A	GROUND ELEVATION (FT)	4188
HOOD TYPE (FROM APP. B)		UTM X COORDINATE (KM)	277123
MINIMUM FLOW (ACFM)		UTM Y COORDINATE (KM)	4710315
PERCENT CAPTURE EFFICIENCY		STACK TYPE (SEE NOTE BELOW)	3
BUILDING HEIGHT (FT)		STACK EXIT HEIGHT FROM GROUND LEVEL	_ (FT) 8
BUILDING LENGTH (FT)		STACK EXIT DIAMETER (FT)	0.5
BUILDING WIDTH (FT)		STACK EXIT GAS FLOWRATE (ACFM)	145
		STACK EXIT TEMPERATURE (DEG. F)	46 (annual avg.)
AIR POLLUTANT EMIS	SIONS		
POLLUTANT CAS NUMBER	EMISSION FACTOR	PERCENT ESTIMATED OR CONTROL MEASURED	ALLOWABLE EMISSIONS
	(SEE NOTE BELOW)	EFFICIENCY EMISSIONS (LBS/HR)	(LBS/HR) (TONS/YR) REFERENCE
PM			
PM-10			
SO2			
co			
NOx			
voc	AP 42	0 81.63	81.63 357.56 Tanks 4.0
LEAD			
Benzene 71-43-2	AP 42	0 4.327E-01	4.327E-01 1.895E+00 Tanks 4.0
Hexane 110-54-3	AP 42	0 7.021E-01	7.021E-01 3.075E+00 Tanks 4.0
Xylenes (mixed isomers) 1330-20-7	AP 42	0 1.796E-01	1.796E-01 7.866E-01 Tanks 4.0
Toluene 108-88-3	AP 42	0 6.123E-01	6.123E-01 2.682E+00 Tanks 4.0
Ethylbenzene 100-41-4	AP 42	0 4.082E-02	4.082E-02 1.788E-01 Tanks 4.0
Naphthalene 91-20-3	AP 42	0 4.566E-05	4.586E-05 2.000E-04 Tanks 4.0
Trimethylpentane (2,2,4) 540-84-1	AP 42	0 1.796E-01	1,796E-01 7,866E-01 Tanks 4.0
Isopropyl Benzene 98-82-8	AP 42	0 2.557E-03	2.557E-03 1.120E-02 Tanks 4.0

STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

NOTES:

SECTION 6: LOADING RACKS

DEQ USE ONLY				
DEQ PLANT ID CODE	DEQ PROCESS CODE	DEQ STACK ID CODE		MARPOROSO I MENERO (MARPORO PERSONALIS MENERO (MENERO PERSONALIS MENERO PERSONALIS MENERO PERSONALIS MENERO P
DEQ BUILDING ID CODE	PRIMARY SCC	SECONDARY SCC		
DEQ SEGMENT CODE				
PART A: LOADING RACK DATA	овоества на выправную не обявать выполняющих не обяваний выполняющих не обяваний выполняющих не обяваний выполняющих не		1907 (Palantan Sangara) (Palanta	manukana keronyuko a jen firanti mataji di kultu sapasa su jen cirin ci si su
PROCESS CODE OR DESCRIPTION	EU#10 . DISTILLATE FUEL OIL LOAD	DING Tier 1/Tier 2 Renewal, 10/9/06		
STACK DESCRIPTION	N/A			
BUILDING DESCRIPTION	N/A			
MANUFACTURER N/A		MODEL N/A	DATE INSTALLED OR LAST MODIFIED	1950*
TYPE OF LOADING	Bottom Loading			
LOADING ARM VAPOR ENCLOSURE	None - open to air, dry	brake coupler		
MATERIAL LOADED	Distillate Fuel Oil			
ANNUAL THROUGHPUT (gallons)	462.966 E 6			
True Vapor Pressure (psia), annual average	0.0044			
MAX. TEMP (F)	54			
AVG TEMP(F)				

^{*} The loading rack was converted from top loading to bottom loading in 1994-1995.
See August 3, 2000 correspondence from Sinclair to Mr. D. E. Hardesty, USEPA region 8

SECTION 6, PAR	RTB EU#10, DIS	STILLATE FUEL OIL LOADING	3 Tier 1/Tier 2 Renewa	al, 10/9/06			
PERCENT FUEL CONS	OPERATING DATA SUMPTION PER QUARTER		OPERATING SCHEDUL	Æ			
DEC-FEB	paratition movement contains in restation in interior		HOURS/DAY	24			
MAR-MAY	25		DAYSWEEK	and a second sec			
JUN-AUG			WEEKS/YEAR	52			
SEP-NOV	25			The state of the s			
	POLLUTION CONTROL EQUIPMEN	Ŧ					
PARAMETER		PRIMARY		SECONDA	RY		
TYPE		N/A		N/A			
TYPE CODE (FROM AP	PP. A)						
MANUFACTURER				performi dentale de articular en desta abracación de alterna de articular en desta abracación de abracación de articular d			
MODEL NUMBER							
PRESSURE DROP (IN.	OF WATER)						
WET SCRUBBER FLOV	V (GPM)]		
BAGHOUSE AIR/CLOTH	RATIO (FPM)						
	VENTILATION AND BUILDING/ARE/	N DATA	STACK D	ATA			
ENCLOSED? (Y/N)		N/A	GROUND ELEVATION (I	FT)		4188	
HOOD TYPE (FROM AP	P. B)		UTM X COORDINATE (K	(M)		277123	
MINIMUM FLOW (ACFM	1)		UTM Y COORDINATE (K	(M)		4710315	
PERCENT CAPTURE E	FFICIENCY		STACK TYPE (SEE NOT	E BELOW)		3	
BUILDING HEIGHT (FT)			STACK EXIT HEIGHT FF	ROM GROUND LEVEL (FT)		[8]	
BUILDING LENGTH (FT)		STACK EXIT DIAMETER	t (FT)		0.5	
BUILDING WIDTH (FT)			STACK EXIT GAS FLOW	VRATE (ACFM)		131	
			STACK EXIT TEMPERAT	TURE (DEG. F)		46	(annual avg.)
	AIR POLLUTANT EMISSIONS						
POLLUTANT	CAS NUMBER	EMISSION	PERCENT	ESTIMATED OR	ALLOWA	BLE EMISSIONS	;
		FACTOR (SEE NOTE BELOW)	CONTROL EFFICIENCY	MEASURED EMISSIONS (LBS/HR)	(LBS/HR)	(TONS/YR)	REFERENCE
РМ				Lambour and Colored Street or West School			- Company of the Comp
PM-10				Part Activities and construction on particular and an extraction of particular and construction of construction of particular and an extraction of particular	Commence of the second	Autora de la constitució de la	Contract securities for a first compression of the security of
SO2							
co							
NOx							
voc		AP 42	0	0.74	0.74	3.26	AP 42
LEAD							
Benzene	71-43-2	AP 42	o o	trivial	trivial	trivial	AP 42
Xylenes (mixed isomers)	1330-20-7	AP 42	0	1.217E-02	1,217E-02	5.330E-02	AP 42
Toluene	108-88-3	AP 42	0	1.114E-02	1.114E-02	4.880E-02	AP 42
Naphthalene	91-20-3	AP 42	0	5.936E-04	5,936E-04	2.600E-03	AP 42

NOTES: STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

SECTION 6: FUGITIVE EMISSIONS

ANNUAL THROUGHPUT (gallons)

DEQ USE ONLY			
DEQ PLANT ID CODE	DEQ PROCESS CODE	DEQ STACK ID CODE	
DEQ BUILDING ID CODE	PRIMARY SCC	SECONDARY SCC	Appropriate State Annual Annua
DEQ SEGMENT CODE			
	unter General par en excellent de mont		mpa-rofusense en roponem en jorden en jorden en jorden de jorden de jorden de jorden en jorden jorden de jorde
PART A: LOADING RACK DATA			
PROCESS CODE OR DESCRIPTION	EU#11 , FUGITIVE EMISSIONS Tier 1/Tier 2 Ren	ewal, 10/9/06	
STACK DESCRIPTION	aanaansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraansuuraa N/A		
BUILDING DESCRIPTION	N/A		
MANUFACTURER N/A	MODE	DATE INSTAILAST MODIF	
MATERIAL TRANSFERRED	Gasoline, Distillate Fuel Oil		

N/A

SECTION 6, PAI	RTB	EU#11 , FUGITIVE EMISSIONS	Tier 1/Tier 2 Renewal, 10/9/				
	OPERATING DATA						
PERCENT FUEL CON	SUMPTION PER QUARTE	R	OPERATING	SCHEDULE			
DEC-FEB	25		HOURS/DAY	24			
MAR-MAY	25		DAYS/WEEK				
JUN-AUG	25		WEEKS/YEA	R 52			
SEP-NOV	25]					
	BOULLITION CONTROL	ECH HOMENT					
PARAMETER	POLLUTION CONTROL	<u>EQUIPMENT</u> PRIMARY		SEC	ONDARY		
TYPE		N/A		N/A			
TYPE CODE (FROM AI	PP. A)			error de la companya del companya de la companya del companya de la companya de l			
MANUFACTURER				Proposition of the Contract of			
MODEL NUMBER						***************************************	
PRESSURE DROP (IN.	OF WATER)			Control of the Contro			
WET SCRUBBER FLO	W (GPM)]	-			
BAGHOUSE AIR/CLOT	H RATIO (FPM)			Comprised the Control of the Control	The transfer of the transfer o		
	VENTS ATION AND DUS	I DINDIADEA BATA		071040471			
ENCLOSED? (Y/N)	VENTILATION AND BUIL	(min)minutes (min)	٦.	STACK DATA		[
HOOD TYPE (FROM AF	36 B)		GROUND ELE			N/A	
MINIMUM FLOW (ACFN	,		UTM X COOR	*			
PERCENT CAPTURE E	•		UTM Y COOR	(SEE NOTE BELOW)			
BUILDING HEIGHT (FT)			1	HEIGHT FROM GROUND LEVEL (I	m		
BUILDING LENGTH (FT		Leading and company of the company o	ī	DIAMETER (FT)	• 1)		
BUILDING WIDTH (FT)		Fast and with all delications from the state of the state	ī	GAS FLOWRATE (ACFM)			
		ровения живониционную в вы выполнения на видения	-	EMPERATURE (DEG. F)			
						bi	
POLLUTANT	AIR POLLUTANT EMISS CAS NUMBER	<u>IIONS</u> EMISSION	PERCENT	ESTIMATED OR	A1 1 (O)A/A	BLE EMISSIONS	
		FACTOR (SEE NOTE	CONTROL EFFICIENCY	MEASURED EMISSIONS	(LBS/HR)	(TONS/YR)	REFERENCE
		BELOW)	J. Francisco-construction	(LBS/HR)	(00000000000000000000000000000000000000	(fearment and the fearment of t
PM							
PM-10							
SO2				-	***************************************		
co							
NOx							
voc		EPA-453/R-95-017	0	0.28	0.28	1.24	EPA-453/R-95-017
LEAD							
Benzane	71-43-2	EPA-453/R-95-017	0	4.772E-03	4.772E-03	2.090E-02	EPA-453/R-95-017
Hexane	110-54-3	EPA-453/R-95-017	0	4.589E-03	4.589E-03	2.010E-02	EPA-453/R-95-017
Xylenes (mixed isomers)	1330-20-7	EPA-453/R-95-017	0	3.167E-02	3.167E-02	1.387E-01	EPA-453/R-95-017
Toluene	108-88-3	EPA-453/R-95-017	0	2.470E-02	2.470E-02	1.082E-01	EPA-453/R-95-017
Ethylbenzene	100-41-4	EPA-453/R-95-017		5.251E-03	5.251E-03	2.300E-02	EPA-453/R-95-017
Naphthalene	91-20-3	EPA-453/R-95-017	0	3.196E-04	3.196E-04	1,400E-03	EPA-453/R-95-017
Trimethylpentane (2,2,4)	540-84-1	EPA-453/R-95-017	0	3.836E-03	3.836E-03	1.880E-02	EPA-453/R-95-017
isopropyi Benzene	98.82-8	EDA_453/B-05-017		5 479E.04	5 4795 04	2 4005 02	EDA 463/B 06 017

NOTES: STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

SECTION 6: SOIL VAPOR EXTRACTION SYSTEM

DEQ USE ONLY			
DEQ PLANT ID CODE	DEQ PROCESS CODE DEQ STACK ID CODE		de former es a facto, a facto a consession provincia con escriptura del provincia companya del provincia con c
DEQ BUILDING ID CODE	PRIMARY SCC SECONDARY SCC		
DEQ SEGMENT CODE			
		kapitat dengangan samagangan hari dalah di semendingan pengangan dalah sebagian dan dalah sebesah dan kangan d	Michel Address einem Michel Anderstein (Anterstein Anderstein (Anterstein Anterstein Anterstein Anterstein Anterstein (Anterstein Anterstein Anterstein (Anterstein Anterstein Anterstein Anterstein Anterstein (Anterstein Anterstein Anterstein Anterstein Anterstein Anterstein (Anterstein Anterstein Anterstein Anterstein Anterstein Anterstein Anterstein Anterstein Anterstein (Anterstein Anterstein Anterstei
PART A: SOIL VAPOR EXTRACTION SYSTEM DA	<u>TA</u>		
PROCESS CODE OR DESCRIPTION	SOIL VAPOR EXTRACTION SYSTEM Tier 1/Tier 2 Renewal, 10/9/06		
STACK DESCRIPTION	See Section 6, Part B		
BUILDING DESCRIPTION	N/A		
MANUFACTURER N/A (Custom Design)	MODEL N/A	DATE INSTALLED OR LAST MODIFIED	2003
TYPE OF UNIT	Soil Vapor Extraction System		
	N/A		
MATERIAL VENTED	Hydrocarbon Vapors from Soil		
VENT FLOWRATE (CFM)	500 (Nominial)		
True Vapor Pressure (psia), annual average	N/A		
MAX. TEMP (F)	Ambient		
AVG. TEMP (F)	Ambient		

SECTION 6, PART B	SOIL VAPOR EXTRACTION SYSTEM	Tier 1/Tier 2 Renewal, 10/9/06			
OPERATING DATA PERCENT FUEL CONSUMPTION PER QUARTE	R	OPERATING SCHEDULE			
DEC-FEB 25	1 .	HOURS/DAY 24			
MAR-MAY 25	Page 1	DAYSMEEK 7			
JUN-AUG 25	i	WEEKS/YEAR 52			
SEP-NOV 25		Automatic consistence and account of the second of the sec			
POLLUTION CONTROL	. EQUIPMENT				
PARAMETER	PRIMARY	SECONDA	₹Y	***************************************	
TYPE CODE (FROM APP. A)	Announce of the contract of th	NA CONTRACTOR CONTRACT			
MANUFACTURER		Control of the Control of Control	nacena consumera interior de la consumera de l Programa de la consumera de la		
MODEL NUMBER	han nguya pun Artin Matin Parin an				
PRESSURE DROP (IN. OF WATER)				CONTROL OF THE PROPERTY OF THE	
WET SCRUBBER FLOW (GPM)	pundo sia fonza del Principio Proprio		j		
BAGHOUSE AIR/CLOTH RATIO (FPM)					
VENTILATION AND BU	LDING/AREA DATA	STACK DATA			
ENCLOSED? (Y/N)	NA separate programment consistency and separate	GROUND ELEVATION (FT)		4188	
HOOD TYPE (FROM APP. 8)		UTM X GOORDINATE (KM)		277130	
MINIMUM FLOW (ACFM)		UTM Y COORDINATE (KM)		4710400	
PERCENT CAPTURE EFFICIENCY		STACK TYPE (SEE NOTE BELOW)		2	
BUILDING HEIGHT (FT)		STACK EXIT HEIGHT FROM GROUND LEVEL (FT)		20	
BUILDING LENGTH (FT)		STACK EXIT DIAMETER (FT)		0.33	
BUILDING WIDTH (FT)		STACK EXIT GAS FLOWRATE (ACFM)		500 (nominal)
		STACK EXIT TEMPERATURE (DEG. F)		ambient (annual avg.)
AIR POLLUTANT EMIS	SIONS				
POLLUTANT CAS NUMBER		PERCENT ESTIMATED OR CONTROL MEASURED EFFICIENCY EMISSIONS (LBS/HR)	ALLOWA (LBS/HR)	ABLE EMISSIONS (TONS/YR)	REFERENCE
РМ					
PM-10	and a second sec				
SO2	description in the control of the co				
со	National Action Control of Contro				
NOx					
VOC	see reference	0 2.06	2.06	9.02	10/14/04 PTC Exemption
LEAD					
Benzene 71-43-2	see reference	0 3.75E-03	3.75E-03	1.64E-02	10/14/04 PTC Exemption
Hexane 110-54-3	see reference	0 6.08E-03	6.08E-03	2.67E-02	see reference note
Xylenes (mixed isomers) 1330-20-7	see reference	0 1.56E-03	1.56E-03	6.82E-03	see reference note
Toluene 108-88-3	See reference	0 5.31E-03	5.31E-03	2.32E-02	see reference note
Ethylbenzene 100-41-4	see reference	0 3.54E-04	3.54E-04	1.55E-03	see reference note
Naphthalene 91-20-3	see reference	0 3.96E-07	3.96E-07	1.73E-08	see reference note
Trimethylpentane (2,2,4) 540-84-1	see reference	0 1.56E-03	1.56E-03	6.82E-03	see reference note
Isopropyl Benzene 98-82-8 reference note: Non-benzene HAP emissions are e	see reference	0 2.22E-05 ne and are not permitted allowable emissions.	2.22E-05	9,71E-05	see reference note

NOTES: STACK TYPE - 01) DOWNWARD; 02) VERTICAL (UNCOVERED); 03) VERTICAL (COVERED); 04) HORIZONTAL; 05) FUGITIVE

EMISSION FACTOR - IN LBS/UNITS. PLEASE USE SAME HOURLY UNITS GIVEN IN FUEL DATA SECTION.

3.0 GENERAL INFORMATION FOR THE FACILITY

3.1 General Description of Facility

The Sinclair Burley Products Terminal receives, stores and distributes petroleum products. The facility was constructed in 1950 and receives petroleum products from the Chevron pipeline (which originates in Salt Lake City, Utah) and stores the petroleum products onsite in any of seven petroleum product storage tanks. There is also one transmix storage tank which is used to store "slop oil" and one prover tank which is used for flow meter calibration. From tankage, the petroleum products are dispensed into carriers, primarily tank trucks, through a two bay loading rack system. Various additives may be blended with the petroleum products prior to dispensing. The carrier then distributes the petroleum products to gas stations, truck stops, airports, farms, etc.

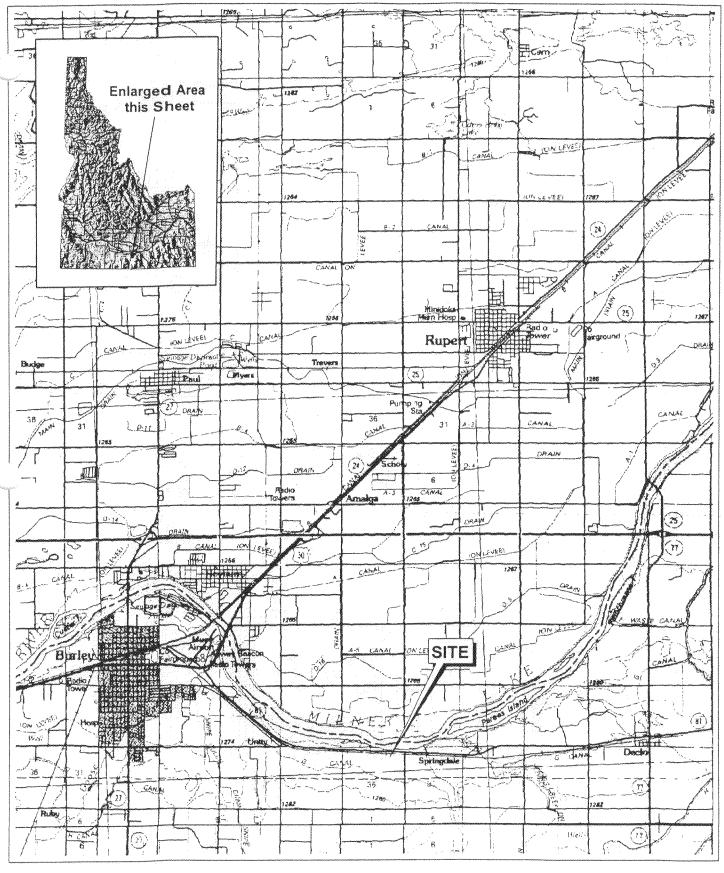
The Sinclair Burley Products Terminal also has installed a Soil Vapor Extraction (SVE) system to remove hydrocarbons from contaminated soil at various locations by the facility.

3.2 Location of Facility

The Burley Products Terminal is located in south central Idaho at 425 East Highway 81 in Burley, Idaho as shown in Figure 3-1. A plot plan of the facility showing the Tier 1 emission sources is provided in Figure 3-2.

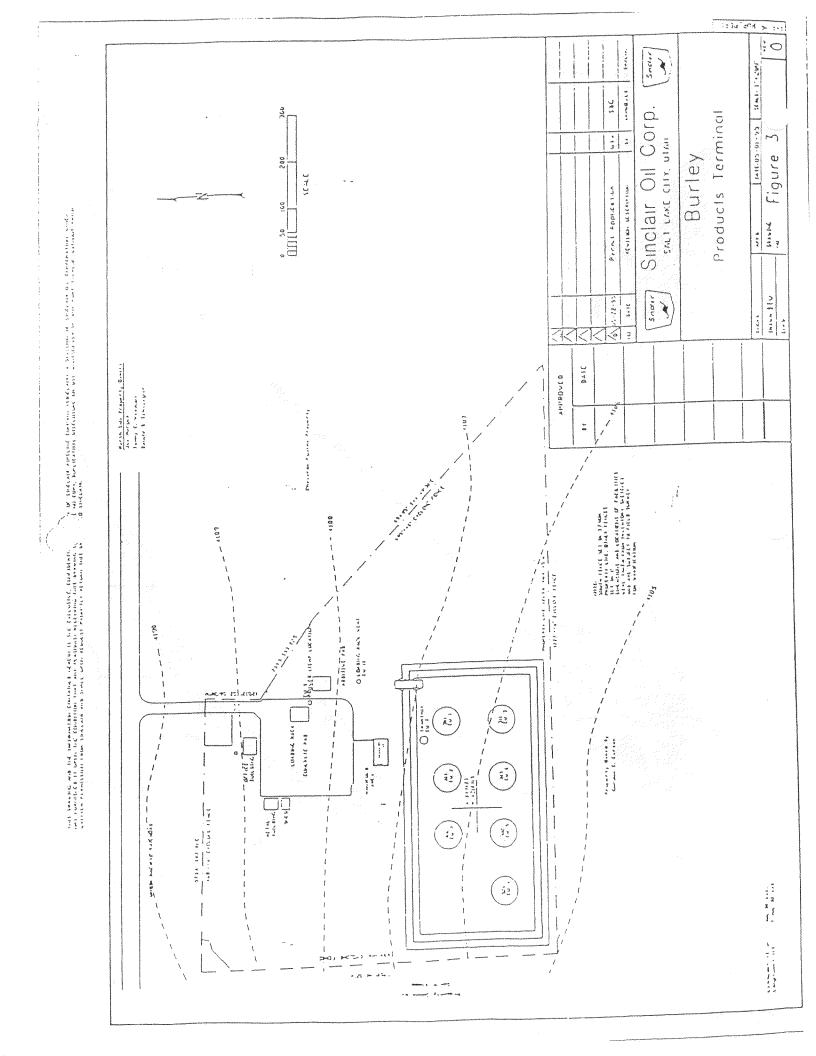
3.3 Description of Product Flow

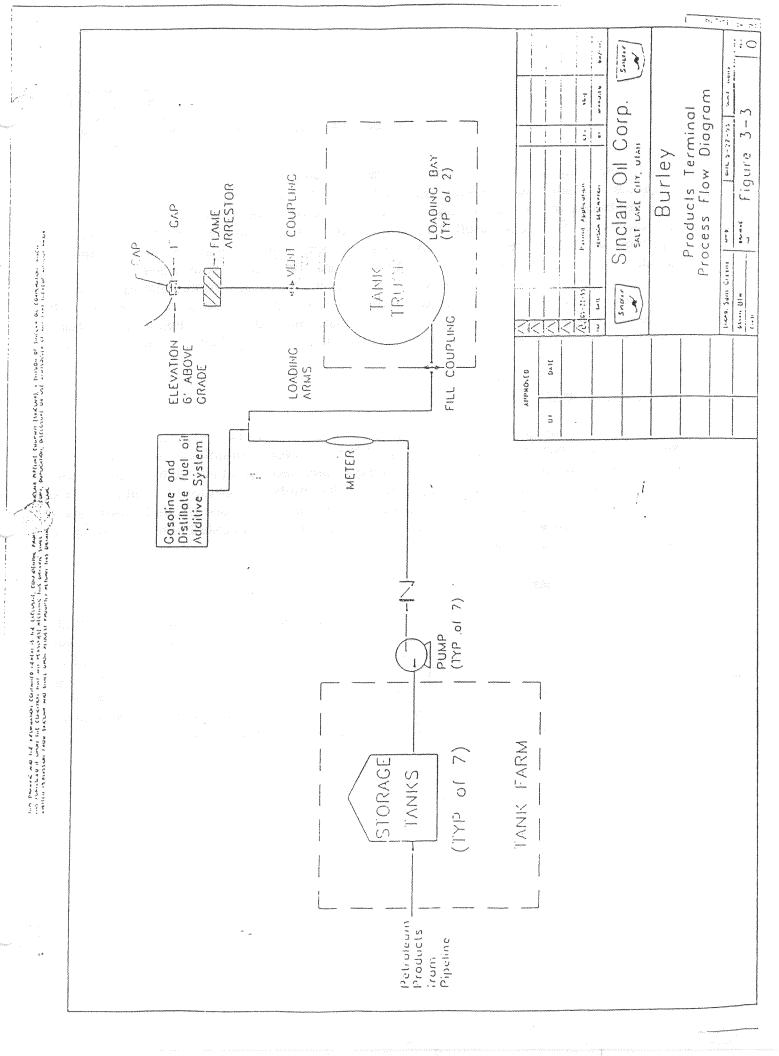
This section describes the flow of petroleum products through the terminal. As shown in the Process Flow Diagram (re: Figure 3-3), petroleum products enter the facility from the pipeline and are directed to the tank farm for storage. The tank farm consists of four gasoline storage tanks, three distillate oil storage tanks and a transmix storage tank. The four gasoline storage tanks are external floating roof type and may be used to store any grade of gasoline (ie. regular unleaded, premium unleaded, etc.) as well as lower vapor pressure petroleum products. The three distillate oil storage tanks are fixed roof type and may be used to store any grade of distillate fuel oil (ie. #2 fuel oil, #1 fuel oil, etc.). The transmix storage tank is fixed roof type and is used to store any grade of gasoline as well as lower vapor pressure petroleum products. The contents of the transmix tank are evacuated with a vacuum truck.





Vicinity Map Burley Terminal Operators Burley, Idaho FIGURE 3.1





The facility is equipped with a two bay, bottom loading rack system for loading petroleum products into tank trucks or other type carriers. When a carrier arrives at the facility, it is directed to one of the loading rack bays where one (or several) of the loading rack arms are attached. Petroleum products are pumped from the tank farm to the loading rack system via a manifolded piping/pump arrangement. Various gasoline and distillate oil additives may be blended into the petroleum products via an in-line blending system. During the filling operation, displaced vapors from the carrier are vented through the vapor collection system and are discharged to atmosphere. Filling of the carrier continues until the desired quantity of product has been transferred. Upon completion of the filling operation, the carrier is disconnected from the loading rack system and exits the facility.

3.4 Calibration of Flowmeters

Periodic calibration of the petroleum products Flowmeters located at the loading rack system is required to ensure accuracy of the inventory control system. Flowmeter calibration is performed by metering a quantity of petroleum product into the Prover Tank, which has a known volume. Comparison of the metered volume of product by the flowmeter with the volume of product transferred to the Prover Tank allows for verification of flowmeter accuracy. If necessary, the flowmeter may be adjusted in order to bring its accuracy within acceptable limits.

3.5 Soil Vapor Extraction System

The Soil Vapor Extraction (SVE) system was installed to remove hydrocarbons from contaminated soil at various locations by the facility. The SVE system was installed under a Permit to Construct Exemption granted by the Division on February 18, 2004 (revised on October 14, 2004). Because the SVE system was exempt from construction permitting and there are no monitoring, recordkeeping and reporting requirements in the Permit to Construction Exemption, Sinclair believes there are no new requirements that need to be incorporated into the Tier 1 and Tier 2 permits regarding the SVE system.

4.0 EXCESS EMISSIONS PROCEDURES

This section provides a description of excess emissions that may occur as a result of startup, shutdown or maintenance activities. The potential emissions from this facility are based upon the allowable petroleum product throughput. Because there are no air pollution control devices associated with this facility, maximum emissions occur when the facility operates at the maximum petroleum product throughput condition. When the facility is being started up or shut down, less than the maximum potential emissions will be released. Therefore no excess emissions due to startup or shut down occur.

The following events have been defined as maintenance activities at this facility:

- Pipe cleaning
- Pipe pressure testing
- Replacement of gasket materials
- Tank cleaning (including grit blasting and water washing)
- Instrument maintenance
- Pump maintenance (including disassembly of pumps)

The release of emissions during maintenance activities will be minimized by utilizing standard maintenance practices for the petroleum industry.

Maintenance activities are non routine and occur on an as needed basis, therefore the frequency of these activities can not be defined. Because of their infrequent nature, the emissions resulting from maintenance activities are considered insignificant.

5.0 EMISSIONS UNIT INFORMATION

This section provides specific information for each Emissions Unit (EU) which is not an insignificant activity.

5.1 Emissions from Emissions Units

Potential air emissions and the analogous product throughputs from the indicated EUs are listed in Chapter 2.0 (re: Storage tanks see DEQ forms Sections 3: Process and Manufacturing Information and Section 5: Storage and Handling of Liquid Solvents and Other Volatile Compounds; Loading rack see DEQ form Sections 6: Loading Racks) and in Appendix: C Fugitive Emissions Calculations.

A summary of maximum potential Volatile Organic Compound (VOC) emissions and Hazardous Air Pollutant (HAP) emissions from each EU and the total from the facility is provided in Table 5.1

5.2 Description of Points of Emission / Definition of Potential Emissions

This section identifies and describes the emissions units in the facility and lists the basis for the maximum potential emissions from each emissions unit.

5.2.1 External Floating Roof Storage Tanks (EU # 1, 2, 3 and 4):

Gasoline grade or distillate fuel oil grade petroleum products can be stored in these tanks. Emissions from these units are a result of standing and withdrawal losses as defined per AP-42 methodology¹. The maximum potential emissions from any one of these tanks occurs when gasoline grade petroleum product is loaded, stored and unloaded at the defined maximum throughput. The maximum throughput for any one of these tanks is defined as the capacity of the pipeline supplying the terminal distributed to three of the four storage tanks (this assumes that one of the four storage tanks is off line for maintenance).

Compilation of Air Pollution Factors, Volume 1 Stationary and Area Point Sources, Section 4.3. AP-42, Fourth Edition, September 1985. USEPA.

Table 5.1 Potential Emissions Summary

EU#	Description	Maximum Potential VOC Emissions (TPY)	Maximum Potential HAP Emissions (TPY)
1	Tank 301	15.17	0.436
2	Tank 304	15.17	0.436
3	Tank 311	15.17	0.436
4	Tank 321	15.17	0.436
5	Tank 402	0.39	0.013
6	Tank 405		0.013
7	Tank 406	- 8 0 .39	0.013
8	Transmix Tank	0.27	0.007
9	Prover Tank	0.26	0.007
10	Loading Rack - gasoline	357.6	9.42
10	Loading Rack - distillate oil	3.26	0.105
11	Fugitive Emissions	aga a - Pa - 1.24	0.332
	Soil Vapor Extraction		
N/A	System	9.02 (Note:1)	0.08 (Note:2)
	Total emissions	433.5	11.7

Note: 1 Per October 14, 2004 Permit to construct Waiver, Section 5.2.

Note: 2 HAP emission estimate is based on:

October 14, 2004 Permit to Construct Waiver for benzene HAP/benzene mass fraction ratioed to gasoline for non-benzene HAP

5.2.2 Fixed Roof Tanks (EU # 5, 6 and 7):

Distillate fuel oil grade petroleum products can be stored in these tanks. Emissions from these units are a result of breathing and working losses as defined per AP-42 methodology. The maximum potential emissions from any one of these tanks occurs when distillate grade petroleum product is loaded, stored and unloaded at the defined maximum throughput. The maximum throughput for any one of these tanks is defined as the capacity of the pipeline supplying the terminal distributed to two of the three storage tanks (this assumes that one of the three storage tanks is off line for maintenance).

5.2.3 Transmix Tank (EU # 8):

The transmix storage tank is fixed roof type and is used to store "slop oil" (ie. off specification petroleum products, residual products from the other storage tanks, water contaminated with petroleum, etc.). Emissions from this unit results of breathing and working losses as defined per AP-42 methodology. The maximum potential emissions from this source occur when gasoline grade petroleum product is loaded, stored and unloaded at the defined maximum throughput.

5.2.4 Prover Tank (EU # 9):

The prover tank is fixed roof type and is used to calibrate the flowmeters in the loading rack system. Emissions from the prover tank occur when the tank is filled and the displaced vapors vent to atmosphere. The maximum potential emissions from this source occur when gasoline grade petroleum product is loaded during meter calibration testing and is dependent upon the number of calibration tests performed.

5.2.5 Loading Rack Vent (EU # 10):

Displaced vapors from carriers, as a result of dispensing product at the two bay loading rack system, are collected and discharged to atmosphere with the loading rack vent. The maximum potential emissions from this source occurs when gasoline grade and distillate grade petroleum products are dispensed at the defined maximum throughput.

5.2.6 Soil Vapor Extraction System

The Soil Vapor Extraction (SVE) system was installed to remove hydrocarbons from contaminated soil at various locations by the facility. An induced draft blower/well system collects hydrocarbon vapors present in the soil and discharges the vapors to atmosphere.

5.3 Emissions Calculations

5.3.1 Tank Emissions Calculation

Calculation of VOC emissions HAP emissions were performed using Tanks Version 4.0 software². The Tanks Version 4.0 outputs for all storage tanks, the transmix storage tank

Storage Tank Emissions Calculation Software, Version 4.0. Emissions Inventory Branch, Office of Air Quality Planning and Standards. USEPA.

and the prover tank are provided in Appendix: A.

5.3.2 Loading Rack Emissions Calculation

The potential emission calculation for the loading rack system was based upon AP-42 methodology³. The calculation is provided in Appendix: B.

5.3.3 Fugitive Emissions Calculation

The potential fugitive emissions calculation was based upon the Protocol for Equipment Leak Emission Estimates ⁴ and AP-42 methodology⁵ and is provided in Appendix: C.

5.3.4 Soil Vapor Extraction System Emissions Calculation

The potential VOC emissions for the SVE system are incorporated by reference from the Division's Per October 14, 2004 Permit to construct Waiver, Section 5.2 (see Appendix D). HAP emissions were based on a HAP/VOC mass fraction of 0.029 (the same HAP/VOC fraction used for EUs 1 through 4).

5.4 Compliance Monitoring / Record Keeping

Compliance with the defined potential emission limits, as listed in Chapter 2.0, will be based upon monitoring the product throughput of the facility. The maximum product throughput limits are defined in Table 5.2.

By limiting the EU throughputs to the values listed in Table 5.2, the facility will not exceed the 25 TPY major source threshold for HAPs.

Compilation of Air Pollution Factors, Volume 1 Stationary and Area Point Sources, Section 5.2, equation (1), AP-42, Fifth Edition, January 1995. USEPA.

⁴ Protocol for Equipment Leak Emission Estimates (EPA-453/R-95-017), Table 2.3, USEPA.

Compilation of Air Pollution Factors, Volume 1 Stationary and Area Point Sources, Section 9.1.3. AP-42, Fourth Edition, September 1985. USEPA.

Table 5.2 Maximum Annual Product Throughput Limits

radic o	2 Maximum Amaa	Product Inroughput Limits
EU#	Description	Maximum EU Throughput (gpy)
1	Tank 301	86,359,000
2	Tank 304	86,359,000
3	Tank 311	86,359,000
4	Tank 321	86,359,000
5	Tank 302	155,599,500
6	Tank 305	155,599,500
7	Tank 306	155,599,500
8	Transmix Tank	38,080
9	Prover Tank	220,200
10	Loading Rack – gasoline	107,310,000
10	Loading Rack - distillate oil	462,996,000
N/A	Soil Vapor Extraction System	N/A

5.4.1 Storage Tank Monitoring (EU # 1 through 8)

The operator will record the quantity of product received in all storage tanks. This information will be compiled on an annual basis to determine product throughput.

5.4.2 Prover (EU # 9)

The operator will compile, on an annual basis, the volume of product transferred to the prover. This information is proportional to the number of flowmeter calibration cycles

during the year.

4.4.3 Loading Rack Monitoring (EU # 10)

The operator will record product throughputs for both bays of the loading rack system. This information will be compiled on an annual basis to determine product throughput.

5.4.4 Process Control

The year-to-date product throughput will be tracked by Sinclair and will be compared to the prorated annual maximum throughput limits. If the year-to-date throughputs are higher than the prorated annual maximum throughputs, Sinclair will make adjustments (if necessary), to ensure compliance at the end of the year.

5.5 Reporting

As currently required by Tier 1 Operating Permit No. T1-030413, Sinclair will continue to report storage tank and loading rack throughputs on an annual basis.

6.0 INSIGNIFICANT ACTIVITIES

In addition to the insignificant activities listed in IDAPA 16.01.01 Section 317, Sinclair is providing a description of emission units and activities that can be performed at the facility which are insignificant (ie. exempt) for purposes of the operating permit program. This listing provides details on selected activities and does not cover all potential insignificant activities that may occur at this facility.

6.1 Presumptively Insignificant Emissions Units

See IDAPA 16.01.01.317.01.a

6.2 Exemption Based on Size or Production Rate

See IDAPA 16.01.01.317.01.b. In addition, the following emission units and activities are exempt from the operating permit program based upon size or production rate.

6.2.1 Petroleum Product Additives

All gasoline additive and distillate fuel oil additive storage, loading and unloading operations at this facility are exempt per IDAPA 16.01.01.317.01.b.i(3): Operation, loading and unloading of VOC storage tanks (including gasoline storage tanks), ten thousand (10,000) gallons capacity or less, with lids or other appropriate closure, vapor pressure not greater than 80 mm Hg at 21 °C. In addition, any fugitive emissions from the additive system are insignificant.

6.2.2 Petroleum Product Sampling

All petroleum product sampling activities at this facility are exempt per IDAPA 16.01.01.317.01.b.i(1): Operation, loading and unloading of VOC storage tanks and storage vessels, with lids or other appropriate closure and less than two hundred sixty (260) gallon capacity (35 ft³), heated only to the minimum extent to avoid solidification if necessary.

6.2.3 Maintenance Activities

Maintenance activities as listed in Chapter 4.0 are defined as insignificant due to their infrequent nature.

7.0 REGULATORY REQUIREMENTS

This section describes the applicable and some of the non-applicable regulatory requirements for this facility.

7.1 Applicable Regulatory Requirement

The only applicable regulatory requirement affecting this facility is listed in IDAPA 16 Title 1 Chapter 1 Sections 525 through 538. These sections establish the criteria for registration of emissions and the payment of fees for Tier 1 facilities. These fees are based on actual annual emissions from the facility.

7.2 Non-Applicable Regulatory Requirements

There are numerous regulatory requirements which do not apply to this facility and to list them all would be a tedious task with minimal benefit. There are regulatory requirements which may apply to other petroleum products storage and distribution facilities which do not apply to this facility. This section lists these non-applicable regulatory requirements for this facility in an effort to illustrate the comprehensive regulatory research undertaken for this permit application. A brief discussion of the basis for non-applicability of these requirements is included.

7.2.1 Standards of Performance for New Stationary Sources (NSPS):

Subpart K - Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction or Modification Commenced After June 11, 1973, and prior to May 19, 1978 does not apply because this facility was constructed or last modified prior to the applicability date.

Subpart Ka - Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction or Modification Commenced After May 18 1978, and prior to July 23, 1984 does not apply because this facility was constructed or last modified prior to the applicability date.

Subpart Kb - Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction or Modification Commenced After July 23, 1984 does not apply because this facility was constructed or last modified prior to the applicability date.

Subpart XX - Standards of Performance for Bulk gasoline Terminals does not apply because this facility was constructed or last modified prior to the applicability date of December 17, 1980.

7.2.2 Maximum Achievable Control Technology Standards (MACT)

Gasoline Distribution MACT does not apply because this facility is not a major source of HAPS (ie. this facility does not have the potential to emit 10 tpy of any individual HAP or 25 tpy of any combination of HAPS).

7.2.3 Ambient Air Impact Analysis

There are no requirements to analyze the ambient air impact of VOC or HAP emissions from existing facilities.

APPENDIX: A STORAGE TANK EMISSIONS CALCULATIONS

Calculation of maximum potential VOC emissions and HAP emissions from all product storage tanks, the transmix storage tank and the prover tank were performed using Tanks Version 4.0 software⁶ which utilizes AP-42 methodology. The emissions reports for these emissions units are provided in this Appendix.

Storage Tank Emissions Calculation Software, Version 4.0. Emissions Inventory Branch, Office of Air Quality Planning and Standards. USEPA.

Tank Identification and Physical Characteristics Emissions Report - Detail Format TANKS 4.0

	Tank 301, pt 1 Teir 2 emissions Burley Idaho Sinlcair Oil Corp. External Floating Roof Tank Tier 2 operating permit renewal	14/14 301 ptt, 14/14 pt2, 14/14 311 pt 3, Tank 321 pt4
Identification	User Identification. City: State: Company: Type of Tank: Description:	

	60.00 838 4 37 00	103.00
Tank Dimensions	Volume (qallons):	Turnovers.

Tumovers: 103.00

WhiteWhite	Double Deck Detail
Shell Color/Shade: Shell Condition:	Roof Characteristics Type: Fitting Category:

lim-Seal System	Welded	Mechanical Shoe	
Tank Construction and Rim-Seal System	Construction	Primary Seal:	Connadan Cont

Rim-mounted	
Secondary Seal.	

Deck Fitting/Status	Quantity
Access halon (24-in, Diam.)/Boiled Cover, Gasketed	1
Automatic Sauge Float Well/Unbotted Cover, Ungasketed	-
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	***
Gauge-Hatch/Sample Well (8-in. Diam.)/Weighted Mech. Actuation, Ungask.	- +-
Roof Drain (3-in. Diameter)/Open	- 4
Roof Leg (3-in. Diameter)/Adjustable, Double-Deck Roofs	- Ç
Rim Vent (6-in. Diameter)/Weighted Mech. Actuation, Gask.)
Stotted Guide-Pole/Sample Well/Ungask. Sliding Cover, w/o Float	· April

Meteorological Data used in Emissions Calculations: Pocatello, Idaho (Avg Atmospheric Pressure = 12.53 psia)

TANKS 4.0 Emissions Report - Detail Format Liquid Contents of Storage Tank

					Liquid			and the second s		AND THE PROPERTY OF THE PROPER	CATALOGRAPHICA CONTRACTOR CONTRAC	-	
		Daily	Daily Liquid Surf.		Bulk				Vapor	Liquid	Vapor		
		Tempe	Temperatures (deg F)		Temp	Vapor P	Vapor Pressures (psia)		TOP S	Mark	Mass	100	Same of the Contract of the Co
Mutua &/Corrocherd	Month	Avg	Min	Max	(deg F)	Avg	Min	Max	Weight	Day	Fract	Wainh	
6	;								Maria			2	1
ついている。	¥	48.21	41.93	54.49	46.37	4.1037	NA	MA	96,0000			92.00	Desting & RAPESTO ACTES Closes
A.A. 4- THINGTHY DOCUMENTS						0.4200	Z/A	N/A	114,2300	0.0151	0.0022	11423	
						0.8343	NIA	A/N	78.1100	0.0188	0 0053	78 11	
Selection of the select						0.0711	N/A	N/A	106.1700	0.0207	0 0005	106 17	
(F) PRINTEG						1,3958	N/A	N/A	86,1700	0.0181	0.0086	8	Option 2 A=6 876 R=1171 17 C=224 41
						0.0324	N/A	N/A	120 2000	0.0022	00000	120 20	_
Dr. Salvan in when						0.0014	N/A	N/A	128.1600	0.0013	0.0000	128 16	
Tolingon													C=211 821
Series Control						0.2263	N/A	N/A	92,1300	0.0972	0.0075	92.13	_
Campana Components						5.5823	N/A	W/A	65,5348	0.7021	0.9737	09.88	
Ayana (-m)						0.0590	N/A	A/A	106.1700	0.0672	0.0013	106 17	Oction 2 A=7 009 B=1462 265 C=215 11
Ayana (O)						0.0460	N/A	A/N	106,1700	0.0573	60000	106 17	-
													1

TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)

Annual Emission Calculations	Market School of the state of t
Rim Seal Losses (Ib):	1,819,6014
Seal Factor A (10-mole/fl-yr.)	0 6000
Seal Factor B (Ib-mole/ft-yr (mph)*n)	0.4000
Average Wind Speed (mph)	10 1167
Seal-related Wind Speed Exponent	1,000
Value of Vapor Pressure Function	6860 0
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psis).	4.1037
Tank Diameter (ft)	90.0000
Vapor Molecular Weight (Ib/Ib-mole)	96.0000
Product Factor.	1.0000
Withdrawal Losses (Ib):	271 4551
Annual Net Throughput (gallyr.)	86,359,000,00
	8
Shell Clingage Factor (bbl/1000 sqft)	0.0015
Average Organic Liquid Density (Ib/gal)	5.6000
Tank Diameter (ft)	60.0000
	1 1 1
Local Comment Cosses (III)	28,251 7303
Value of Vapor Pressure Function	0.0989
Vapor Molecular Weight (Ib/Ib-mole)	66.0000
Product Factor	1.0000
Tot. Roof Fitting Loss Fact (Ib-mole/yr)	4,328,7407
Average Wind Speed (mph)	10,1167

Section of the sectio				Roof Fitting Loss Factors		
Access Hafth (Main Diam Machael Course Confession	(Deliver Can) also	Quantity	KFa (ib-mole/yr)	KFb (lb-mole/(yr mph^n))	E	I nessas (In.)
Automatic Gauge Float Well/Linbolted Cover Linguistics	COURT CONSTITUTION	igen.	58	000	00'0	10 4425
Vacuum Breaker (10-in, Diam IMeighled Mech. Actuation, Gack	Biothled Mech Actuation Gark		14.00	5,40	1.10	394 9189
Gauge-Hatch/Sample Well (8-in, L	Gauge HistorySample Well (8-in, Diam, Weighted Mech. Actuation Undask	~ *	07.0	1.20	3 60	89 7811
Roof Drain (3-in, Diameter)/Open		m: w	2.30	880	00 :	15,0111
Roof Leg (3-in. Diameter)/Adjustable, Double-Deck Roofs	ale, Double-Deck Roofs	- 5	3 6	17.0	1/0	47,9960
Rim Vent (6-in. Diameter/Weighted Mech. Actuation, Gask	d Mech. Actuation, Gask	2	0.02	20.00	J .	98 0142
Siothed Guide-Pole/Sample Well/Ungask, Sliding Cover, w/o Float	ngask. Sliding Cover, w/o Float	. 400	43.00	270.00	3 5	9.2557
				7	9	2018 CBC 17
Total Losses (lb)	30,342.7867					

.

TANKS 4.0 Emissions Report - Detail Format Individual Tank Emission Totals

Annual Emissions Report

Components	The second secon		Losses(lbs)		
10,000	Rim Seal Loss	Withdrawal Lock	Dack Eitting Loss		The state of the s
ことにいることには、これには、これには、これには、これには、これには、これには、これには、これ	4 040 00	0002	CCCV LINE TOSS	CY OCCU	lotal Emissions
Ranzono	0.8.0,	2/1.46	28,251.73	00.0	20 242 7g
211271120	9.69	5.10	150.51		0 0 0 0 0
Ellylibenzene	0.91	5.62	4 4 4 2	The second of th	10.00
Hexane (-n)	45.04	20:0	2		20.66
To the first of the second	10.01	LD:4	242.44		76.090
Tablillatene	00.0	0.35	100	The second secon	1000
Xylene (-m)	SPC	*****	10.00		78.0
Video Col	200	h7.01	38.08		58 73
	3	15,55	25.27	The second secon	1. 0.
Toluene	13.59	26 30	244 06		47.45
2.24-Trimathylpantana	0000	20.03	8		251.04
CALLES CONTRACTOR CONT	3.37	25.4	60.86		70 00
Isopropyl benzene	000	080	0.88	The contract of the contract o	0.00
Inidantified Components	36. 76.6. 7	2000	0.00	00.0	.33
	1,771.70	190.59	27,508.72	900	29 471 06

TANKS 4.0 Emissions Report - Detail Format Tank Identification and Physical Characteristics

	Tank 302 pt 5 tier 2 emissions	Burley	Idaho	Sinclair Oil Corp.	Vertical Fixed Roof Tank	Tank 302 pt5, Tank 305 pt 6, Tank 306 pt
nontrance of the second	User Identification	City	State	Company	Type of Tank:	Description

Tank Dimensions	
Shell Height (ft)	40.00
Diameter (ft):	60.00
Liquid Height (ft)	39.00
Avg. Liquid Height (ft):	20.00
Volume (gallons):	825,024.00
Turnovers	189.00
Net Throughput (gallyyr):	155,599,500.00
Is Tank Heated (v/n)	Z

189.00	155,599,500.00		White/White	Good	White/White	Good		Cone	2.00	0.07
Turnovers	Net Throughput (gal/yr): Is Tank Heated (y/n):	Paint Characteristics	Shell Color/Shade: Wr	Shell Condition: Go	Roof Color/Shade	Roof Condition: Go	Roof Characteristics	Type: Co	Height (#)	Slope (ft/ft) (Cone Roof):

Height (ft.) Slope (ft/ft) (Cone Roof): Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig):	2.00	0.07		-0.03	0.03
	Tegar (=)	Slope (ft/ft) (Cone Roof).	Breather Vent Settings	Vacuum Settings (psig)	Pressure Settings (psig):

Meteorological Data used in Emissions Calculations: Pocatello, Idaho (Avg Atmospheric Pressure = 12.53 psia)

TANKS 4.0 Emissions Report - Detail Format Liquid Contents of Storage Tank

Pidpid	Bulk Vapor Liquid Vapor	Temperatures (deg F) Temp. Vapor Pressures (psia) Mol Mass Mass Mol Basis for Vapor Pressure	Max (deg.F) Avg Min Max Weight Fract. Fract. Weight	0.0035 0.0054 130.0000 (88.00	0.0014 0.0010 0.0017 0.0008 128.16 Option 2: A=7.1463, B=1831.571,	0.1834 0.2774 92.1300 0.0002 0.0150 92.13	0.0041 0.0041 131,3375 0.9972 0.9679 188,32	0.0590 0.0465 0.0743 106.1700 0.0006 0.0118 106.17 Option 2. A=7,009, B=1462, 266, C=215.11	
		Vapor Pressures (Avg. Min.						
Liquid	Bulk	Temp.	(deg F)		O	O	O	O	
				54.49					
	Liquid Surf.	atures (deg F)	Min	41.93					
	Daily	Тептрег	Avg.	48.21					
			Month	Ä					
			Mixtura/Component	Distillate fuel oil no. 2	naphthalene	Toluene	Unidentified Components	Xylera (-m)	

98 8055 58,433 6233 0 0001 0 0448 0 9953	58, 433, 6233 60,0000 20, 6667 40,0000 20,0000 0,6667	.0 6667 2 0000 0 0700 30,0000	0.0001 130.0000 0.0044 507.8766 46.3542	10.731 506.0442 0.1700 0.1700 1,371,0030	0.0448 25.1200 0.0019 0.0000 0.0044 0.0035 0.0054 507.8766 501.5966 514.1566 25.8250	0.9953 0.0044 20.6667
Annuel Emission Calculations Standing Losses (Ib) Vapor Spoere Volume (cu.ft) Vapor Density (Ibricu.ft) Vapor Spece Expansion Factor Vented Vapor Saturation Factor	Tank Vapor Space Volume Vapor Space Volume (cu fi) Tank Diameter (fi) Vapor Space Outage (fi) Tank Shell Height (fi) Average Liquid Height (ft) Roof Outage (ft)	Roof Outage (Cone Roof) Roof Outage (f) Roof Height (f) Roof Stope (ftff) Shell Redius (ft)	Vapor Density Vapor Density Vapor Density (Ibrou ft) Vapor Molecular Weight (Ibrib-mole). Vapor Pressure in Daily Average Liquid Surface Temperature (psia) Daily Average Ambient Temp (deg. R)	Ideal Gas Constant R (psia cuf / (broud-deg R)) Liquid Bulk Temperature (deg, R) Tank Paint Solar Absorptance (Shell) Tank Paint Solar Absorptance (Roof) Daily Total Solar Insufation Factor (Blufsoff day)	Vapor Space Expansion Factor Vapor Space Expansion Factor Daily Vapor Pressure Range (bas) Daily Vapor Pressure Range (pas) Breather Vent Press, Setting Range(pas) Vapor Pressure at Daily Average Liquid Surface Temperature (pasi) Vapor Pressure at Daily Minimm Liquid Surface Temperature (pasi) Vapor Pressure at Daily Maximum Liquid Surface Temperature (pasi) Daily Ang Liquid Surface Temp (deg R) Daily Max Liquid Surface Temp (deg R) Daily Max Liquid Surface Temp (deg R) Daily Max Liquid Surface Temp (deg R) Daily Ambient Temp Range (deg R)	Versted Vapor Saturation Factor Vented Vapor Saturation Factor Vapor Pressure at Daily Average Liquid Surface Temperature (psia) Vapor Space Outage (fi)

TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)- (Continued)

582 3016	130,0000		0.0044	155,599,500.0	000	189 0000	0.3254	825,024,0000	39,0000	80,0000	1,0000	781.1070
Working Losses (Ib)	Vapor Molecular Weight (Ib/lb-mole)	Vapor Pressure at Daily Average Liquid	Surface Temperature (psia)	Annual Net Throughput (gallyr.)		Annual Tumovers.	Jumoner Fedor	Maximum Liquid Volume (gal)	Maximum Liquid Height (ft)	Tank Diameter (ft)	Working Loss Product Factor	Total Losses (Ib)

Vertical Fixed Roof Tank Burley, Idaho

TANKS 4.0 Emissions Report - Detail Format Individual Tank Emission Totals

Annual Emissions Report

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	682.30	98.81	781.11
naphthalene	0.53	80.0	0.61
Toluene	10.26	1.49	11.74
Xylene (-m)	8.02	9;	9.18
Xylene (-o)	3.12	0.45	3.58
Unidentified Components	660.37	95.63	756.00
			And desirable the second secon

Vertical Fixed Roof Tank Burley, Idaho

Emissions Report - Detail Format Tank Identification and Physical Characteristics TANKS 4.0

Tmix pt 8 tier 2 emissions Burley Idaho Sinclair Oil Corp. Vertical Fixed Roof Tank transmix tier 2 emissions	20.00 6.00 18.00 5.00 3,808.00 10.00 38,080.00	WhiteMhite Good WhiteMhite Good	Cone 2.00	-0.03
Identification User Identification: City: State: Company: Type of Tank: Description:	Tank Dimensions Shell Height (ft): Diameter (ft): Liquid height (ft): Avg. Liquid Height (ft): Volume (gallons): Turnovers: Net Throughput (gal/yr): Is Tank Heated (y/n):	Paint Characteristics Shell Color/Shade: Shell Condition: Roof Color/Shade: Roof Condition:	Roof Characteristics Type: Height (ft): Slope (ft/ft) (Cone Roof):	Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig):

Meteorological Data used in Emissions Calculations: Pocatello, Idaho (Avg Atmospheric Pressure = 12.53 psia)

Vertical Fixed Roof Tank Burley, Idaho

TANKS 4.0 Emissions Report - Detail Format Liquid Contents of Storage Tank

Basis for Vapor Pressure Calculations	Option 4: RVP=10, ASTM Slope=3 Option 2: A=6 8118, B=1257, B4, C=220.74 Option 2: A=6.905, B=1211.033, C=220.79 Option 2: A=6.975, B=124.24.255, C=213.21 Option 2: A=6.975, B=1424.255, C=224.41 Option 2: A=6.953, B=1460.733, C=207.78 Option 2: A=7.1463, B=1831.571, C=211.821 Option 2: A=6.954, B=1344.8, C=219.48	Option 2: A=6,998, B=1462,266, C=215,11 Option 2: A=6,998, B=1474,679, C=213,69
Mol	92.00 114.23 78.11 106.17 86.17 120.20 128.16 92.13 89.60	106.17
Vapor Mass Fradi	0.0022 0.0053 0.0005 0.0006 0.0006 0.0000 0.0000	0.00013
Liquid Mass Frad.	0.0151 0.0168 0.0207 0.0181 0.0022 0.0013 0.0972	0.0672
Vapor Mol. Weight	66,0000 114,2300 78,1100 106,1700 86,1700 120,2000 128,1600 92,1300 65,5348	106.1700
Max	4,6545 0,5071 1,0003 0,0833 1,6547 0,0415 0,0019 0,2774 5,5594	0.0743
Vapor Pressures (psia)	3.6067 0.3458 0.6919 0.0562 1.1713 0.0252 0.0010	0.0361
Vapor P	4.1037 0.4200 0.8343 0.0711 1.3958 0.0324 0.0014	0.0590
Liquid Bulk Temp (deg F)	46.37	
Max	8.4. 8.4.	
Daily Liquid Surf. Temperatures (deg F)	A. C.	
Daily Temper	48.21	
Month	₹	
Mixture/Component	Casoline (RVP 10) 2.4-Trimethylpentane Benzene Ethylbenzane Hexane (-n) Isopropyl benzene naphthalene Toluene Vindentified Components	Xyteras (-0)

TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)

Vertical Fixed Roof Tank Burley, Idaho

303.9487 442.9646 0.0497 0.1667 0.2269	42 9646 6 6000 15 6667 20 0000 5 0000 0 6667 2 0000 0 6700 3 0000	0.0497 66 0000 4 1037 507 8766 46,3542 10.731 506 0442 0.1700 1,371,0030	0.1667 25.1200 1.0479 0.0600 4.1037 3.6067 4.6545 507.8766 501.5966 514.1566 25.8250	0.2269 4.1037 15.6667
Arrual Emission Calculations Slanding Losses (Ib) Vapor Space Volume (ou ft) Vapor Density (Ibro. ft) Vapor Space Expension Factor Vented Vapor Saturation Factor	Tank Vapox Space Volume Vapox Space Volume Vapox Space Volume Tank Diameter (i) Vapox Space Outage (ii) Tank Shell Height (ii) Average Liquid Height (ii) Roof Outage (fin) Roof Outage (fin) Roof Height (iii) Roof Height (iii) Roof Stope (fin) Shell Radus (iii)	Vapox Density Vapox Density Vapox Molecular Weight (Bhb-mola) Vapox Molecular Weight (Bhb-mola) Vapox Pressure at Davily Average Liquid Surface Temperature (Bris) Davily Average Ambient Temp (deg R) Davily Average Ambient Temp (deg R) Ideal Gas Constant R (pala cuff (Ib-mol-deg R)) Liquid Builk Temperature (deg R) Tank Paint Solar Absorptance (Shell) Tank Paint Solar Absorptance (Roof) Davily Total Solar hasulation Facor (Bru/soff day)	Vapor Space Expansion Factor Vapor Space Expansion Factor Daily Vapor Temperature Range (deg R) Daily Vapor Pressure Range (ptg.) Berether Verti Press. Setting Range(ptg.) Vapor Pressure at Daily Average Liquid Surface Temperature (psia) Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia) Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia) Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia) Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia) Daily Awa Liquid Surface Temp (deg R) Daily Max Liquid Surface Temp (deg R) Daily Ambiert Temp Range (deg R)	Vertied Vapor Saturation Factor Vertied Vapor Saturation Factor Vapor Pressure at Daily Average Liquid Surface Temperature (psia) Vapor Space Outage (ft)

3/27/2002 1:01:44 PM

TANKS 4.0

Working Losses (lb).	245 5652	
Vapor Molecular Weight (Ib/Ib-mole)	99	
Vapor Pressure at Daily Average Liquid		
Surface Temperature (psia)	4 1037	
Annual Mat Throughput (gallyr.)	38,080,0000	
Amoust Tumovers	10,0000	
Lumovar Factor	1000	
Maximum Liquid Volume (pal)	3,808,0000	
Maximum Liquid Height (ft)	18,0000	
Tank Diameter (ft)	6.0000	
Working Loss Product Factor	1,0000	
Total Losses (Ib)	540 5130	

Emissions Report - Detail Format Individual Tank Emission Totals TANKS 4.0

Annual Emissions Report

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Ethylbenzene	0.12	0.15	70.0
Hexane (-n)	2.11	2.61	4.72
naphthalene	00.00	00.0	
Toluene	1.83	2.27	7
Xylene (-o)	0.22	0.27	0.49
Xylene (-m)	0.33	0.41	0.74
2,2,4-Trimethylpentane	0.53	0.65	- C
Isopropyl benzene	100	0.01	0.01
Unidentified Components	239.11	295.96	535.06
Gasoline (RVP 10)	245.57	303.95	549.51
Benzene	£6.	1.62	2.93

Emissions Report - Detail Format Tank Identification and Physical Characteristics TANKS 4.0

prover tk pt 9 Burley Idaho	Sinclair Oil Corp. Vertical Fixed Roof Tank prover tier 2 emissions
User Identification:	Company.
City:	Type of Tank:
State:	Description:

Identification

	9	88 6	100	2.00	734 00	30008	220.200.00	4
Tank Dimensions	Shell Height (ft)	Diameter (ft):	Liquid Height (ft)	Avg Liquid Height (ft)	Volume (gallons):	Turnovers	Net Throughput (gallyrr)	Is Tank Heated (u/n).

300	5.00	2.00	734.00	300.00	220,200,00	Z		White/White	Good	White/White	Good	
(11)	Light (A)	Avg. Liquid Height (ft):	Volume (gallons):	lumovers	Net Throughput (gallyr):	Is Tank Heated (y/n):	Paint Characteristics	Shell Color/Shade	Shell Condition	Roof Color/Shade	Roof Condition	

		2.00	0.80	
	Cone			
Roof Characteristics	Type	Height (ft)	Slope (ft/ft) (Cone Roof)	6 ·

	-0.03	0.03
Breather Vent Settings	Vacuum Settings (psig)	Pressure Settings (psig).

Meteorological Data used in Emissions Calculations: Pocatello, Idaho (Avg Atmospheric Pressure = 12.53 psia)

TANKS 4.0 Emissions Report - Detail Format Liquid Contents of Storage Tank

AND			Liquid	Company of Commission and Commission of Comm	THE RESERVE THE PROPERTY OF THE PERSON OF TH	- Land and the control of the contro	Transmission of the American Statement of the American	NAMES AND ADDRESS OF THE PERSON NAMES OF THE P			
Daily Liquid Surf.	£.		¥na.				Vapor	Liquid	Vapor		
Temperatures (deg F)	,,,,,,,		Temp.	Vapor P	Vapor Pressures (psia)		Mol	Mass	Mass	MOM	Basis for Vapor Pressure
Avg. Min.	- 1	Max	(deg F)	Avg	Min.	Max	Weight	Frad	Fred	Weight	Calculations
48.21 41.93		54.49	46.37	4.1037	3.6067	4.6545	00000.99			92.00	Option 4. RVP=10. ASTM Slooe=3
				0.4200	0.3458	0.5071	114,2300	0.0151	0.0022	114.23	Option 2, A=6,8118, 8=1257,84, C=220,74
				0.8343	0.6919	1,0003	78.1100	0.0188	0.0053	78.11	Option 2: A=5.905, B=1211,033, C=220.79
				0.0711	0.0562	0.0893	106,1700	0.0207	0.0005	106.17	Option 2, A=6.975, B=1424,255, C=213,21
				1,3958	1.1713	1.6547	86,1700	0.0181	9800.0	88.17	Option 2, A=6,876, B=1171,17, C=224,41
				0.0324	0.0252	0.0415	120.2000	0.0022	00000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
				0.0014	0.0010	0.0019	128,1600	0.0013	0.0000	128.16	Option 2: A=7,1463, B=1831,571,
											C=211.821
				0.2263	0.1834	0.2774	92,1300	0.0972	0.0075	92.13	Option 2. A=6.954, B=1344.8, C=219.48
				5.5823	5.5593	5, 5594	65,5348	0.7021	0.9737	89.60	
				0.0590	0.0465	0.0743	106,1700	0.0672	0.0013	186.17	Option 2: A×7,009, B=1462,266, C×215 11
				0.0460	0.0361	0.0581	106,1700	0.0573	6000 0	106.17	Option 2; A=6,998, B=1474,679, C=213.69

.0 Detail Format

Vertical Fixed Roof Tank Burley, Idaho

	137 5255	24 6308	0.0497	0.1667	0.4963		91,6298	2,000	4 6667	9,000	2,0000	0.6667		0.6567	3 (300)	2 BOTO	2.5000		70%97	86,000		4.1037	507.8766	46.3542		10,731	506.0442	355	3	1,371,0030		0.1567	25.1200	104/9	One Control of	4.1037	2 6000	900	4.6545	507.8766	501.5966	514.1566	nezo'ez	6	U 4963	4,1037	4 0000/
Amual Emission Calculations	Standing Losses (lb)	Vapor Space Volume (cu fl)	Vapor Density (fb/cu/fl)	Vapor Space Expansion Factor	Versed Vapor Saturation Factor	Tank Vapor Space Volume	Vapor Space Volume (ou ft)	Tank Diameter (ft):	Vapor Specs ⊜iage (ft)	Tank Shall Height (A)	Average Liquid Height (ft)	Mood Outage (ft)	Roof Outsos (Cone Roof)	Rod Outsoe (#)	Roof Height (R)	Roof Slope (PM)	Shell Radius (ft)	Vapor Density	Vapor Density (Ib/ou ft)	Vapor Molecular Weight (Ib/Ib-mole)	Vapor Pressure at Daily Average Liquid	Surface Temperature (psia)	Daily Avg Liquid Surface Temp. (deg. R.)	Daily Average Ambient Temp. (deg. F):	Messicas Constant R	(psie am / (ib-mol-deg R))	Later Dark Character at a control of the	Tack Pain Sciar Absorbance (Roch		Factor (Blu/sqf day)	Vapor Space Expansion Factor	Vapor Space Expansion Factor	Delly Vapor (emperature Hange (deg. R)	Breather Very Press Setting Regulation	Vapor Pressure at Daily Average Liquid	Surface Temperatura (para)	Suffice Temperature (paid)	Vapor Pressure at Daily Maximum Liquid	Surface Temperature (psis)	Daily Avg Liquid Surface Temp (deg R)	Usiny Min Lydud Surface Temp (deg R)	Daily Max, Erduid Surface Temp. (deg R). Daily Ambient Temp. Rance (dec. R).	· Con · 海をおげるカー・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・・	Verted Vapor Saluration Factor	Vapor Pressure 91 Daily Average Liquid	Surface Temperature (psia) Vanor Spare Outson (2)	(11) pharms are not some

TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)

TANKS 4.0 Emissions Report - Detail Format Detail Calculations (AP-42)- (Continued)

Vertical Fixed Roof Tank Burley, Idaho

Vapor Molecular Weight (Bith-mole) Vapor Pressure at Daily Average Liquid Vapor Pressure at Daily Average Liquid Surface Temperature (sisis) Annual Net Throughbol (gailyr) Annual Net Throughbol (gailyr) Annual Net Throughbol (gailyr) Annual Liquid Volume (gailyr) Maximum Liquid Volume (gail) Tak Osoma Maximum Liquid Height (ft) S 0000 Working Loss Prioduct Factor 10000	378,6656	
2220,	0000 99	
220,	4.1037	
.,	220,200,0000	
	300,0000	
-	0.2667	
	734,0000	
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86.000
4 1037
220,200,0000
300,0000
0.2667
734,0000
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1 8000

TANKS 4.0 Emissions Report - Detail Format Individual Tank Emission Totals

Annual Emissions Report

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Gasoline (RVP 10)	378.67	137.53	516.19
Ethylbenzene	0.19	0.07	0.26
Hexane (-n)	3.25	2	4.43
naphthalene	00.0	0.00	00.00
Toluene	2.83	1.03	3.86
Xylene (-0)	0.34	0.12	0.46
Xylene (-m)	FG C	0.19	69.0
2,2,4-Trimethylpentane	0.82	0:30	*-
Isopropyl benzene	S _O	00.00	0.01
Unidentified Components	368.71	133.91	502.62
Benzene	2.02	0.73	2.75
			The state of the s

APPENDIX: B LOADING RACK EMISSIONS CALCULATIONS

Calculation of potential VOC emissions from the loading rack system were based upon AP-42 methodology⁷. Calculation of maximum potential HAP emissions from the loading rack system were based upon the maximum potential VOC emission rate speciated for HAPS. Speciation of HAPs was obtained from the vapor mass fractions listed in the Tanks Version 4.0 output (re: Appendix: A). The maximum potential emission calculations for gasoline loading and distillate fuel oil loading follow.

Compilation of Air Pollution Factors, Volume 1 Stationary and Area Point Sources, Section 5.2, equation (1), AP-42, Fifth Edition, January 1995. USEPA.

Sinclair Oil Corp., Burley Terminal Tier 1 Renewal Rev. 0, May 16, 2003 Loading Rack Emissions EU#11

Facility Input:

Gasoline

Distillate Fuel Oil

7000 BPD 30202 BPD

2555000 BPY 11023714 BPY

Gasoline:

Annual Throughput Annual Throughput 2555000 BPY 107310 M gpy

Formula:

Loading Losses (lb/1000 gal) = (12.46)(S)(P)(M)/T)

Re: AP-42

Where:

S = saturation factor

P = True Vapor Pressure (psia) M = Molecular Weight of Vapor T = Liquid Temperature (deg. R)

MW

Pvap

Saturation Factor

4.1037 psia

Temperature

506.4 deg. R 6.6641 lb/M gal 357.56 TPY

Emission Factor
Total VOC emission rate

	Component	Vapor Mass	Emission	HAP Emission
		Fraction	Rate (TPY)	Rate (TPY)
1	Benzene	0.0053	1.8951	1.8951
2	Hexane	0.0086	3.0751	3.0751
3	Xylene-o	0.0009	0.3218	0.3218
4	Xylene-m	0.0013	0.4648	0.4648
5	Xylene-p (inc. with o & m)	0.0000	0.0000	0.0000
6	Toluene	0.0075	2.6817	2.6817
7	Ethylbenzene	0.0005	0.1788	0.1788
8	Naphthalene	0.0000	0.0002	0.0002
9	Trimethylpentane (2,2,4)	0.0022	0.7866	0.7866
10	Curnene	0.0000	0.0112	0.0112
11	Non HAP gasoline	0.9737	348,1489	
-	SUBTOTAL	1.00	357.56	9.42

Distillate Fuel Oil

Annual Throughput

Annual Throughput

11023714 BPY 462996 M gpy

Formula:

MW

Pvap

Loading Losses (lb/1000 gat) = (12.46)(S)(P)(M)/T)

Re: AP-42

Where:

S = saturation factor

P = True Vapor Pressure (psia) M = Molecular Weight of Vapor T = Liquid Temperature (deg. R)

130

Saturation Factor

0.0044 psia

506.4 deg. R

Temperature Emission Factor

0.0141 lb/M gal 3.26 TPY

Total VOC emission rate

	Component	Vapor Mass	Emission	HAP Emission
		Fraction	Rate (TPY)	Rate (TPY)
1	Benzene	0	0.0000	0.0000
2	Hexane	0	0.0000	0.0000
3	Xylene-o	0.00458	0.0149	0.0149
4	Xylene-m	0.01179	0.0384	0.0384
5	Xylene-p (inc. with o & m)	0	0.0000	0.0000
6	Toluene	0.01499	0.0488	0.0488
7	Ethylbenzene	0	0,0000	0.0000
8	Naphthalene	0.00079	0.0026	0.0026
9	Trimethylpentane (2,2,4)	0	0.0000	0.0000
10	Cumene	0	0.0000	0.0000
11	Non HAP Fuel oil	0.96785	3.1534	***************************************
	SUBTOTAL	1.001	3.26	0.1047

SBG/sbg 5/16/03

APPENDIX: C FUGITIVE EMISSIONS CALCULATIONS

The potential fugitive emissions calculation was based upon the Protocol for Equipment Leak Emissions Estimates (EPA-453/R-95-017, Table 2-3) and AP-42 methodology and is listed in this Appendix.

Sinclair Oil Corp., Burley Terminal Tier 2 Renewal Rev. 1, March 27, 2002 Fugitive Emissions EU#12

Re: Protocol for Equipment Leak Emission Estimates (EPA-453/R-95-017, Table 2-3) AP-42, 4 ed. (Fugitive Emission Factors, Table 9.1-2) Fugitive VOC emissions Source Pump Valves Flanges Drains Others VOC Emission Rate (TPY) Seals 1 Gasoline service 200 400 8 30 Quantity 0.00119 0.0000176 0.000287 0.0377118 Emissions Factor 0.0000948 (lb/hr-source 0.07 (TPY) 0.0416976 0.0830448 0.0308352 0.9198 1.11 Emissions 2 Distillate oil service 100 300 Quantity 0 30 0.0000948 Emissions Factor (lb/hr-source) 0.00119 0.0000176 0.07 0.000287 (TPY) 0.026061 0.0415224 0.0231264 0 0.0377118 0.13 Emissions TOTAL VOC EMISSIONS 1.24

SBG/sbg 3/27/02

Fugitive emissions - gasoline service

	Component	Liquid Mass	VOC Emission	HAP Emission
		Fraction	Rate (TPY)	Rate (TPY)
1	Benzene	0.0188	0.021	0.021
2	Hexane	0.0181	0.020	0.020
3	Xylene-o	0.0573	0.064	0.064
4	Xylene-m	0.0672	0.075	0.075
5	Xylene-p (inc. with o & m)	0.0000	0.000	0.000
6	Toluene	0.0972	0.108	0.108
7	Ethylbenzene	0.0207	0.023	0.023
8	Naphthalene	0.0013	0.001	0.001
9	Trimethylpentane (2,2,4)	0.0151	0.017	0.017
10	Cumene	0.0022	0.002	0.002
11	Non HAP Gasoline	0.7021	0.782	
	TOTAL	1.0000	1.113	0.332

Fugitive emis	sions - fuel oil service				
	Component	Liquid Mass		VOC Emissi	HAP Emission
		Fraction		Rate (TPY)	Rate (TPY)
1	Benzene		0.0000	0.0000	0.0000
2	Hexane		0.0000	0.0000	0.0000
3	Xylene-o		0.0003	0.0000	0.0000
4	Xylene-m		0.0006	0.0001	0.0001
5	Xylene-p (inc. with a & m)		0.0000	0.0000	0.0000
6	Toluene		0.0002	0.0000	0.0000
7	Ethylbenzene		0.0000	0.0000	0.0000
8	Naphthalene		0.0017	0.0002	0.0002
9	Trimethylpentane (2,2,4)		0.0000	0.0000	0.0000
10	Cumene		0.0000	0.0000	0.0000
11	Non HAP Fuel Oil		0.9972	0.1281	
	TOTAL		1.0000	0.1284	0.0004

TOTAL VOC EMISSION RATE (TPY)=
TOTAL HAP EMISSION RATE (TPY)=

1.24

0.33

APPENDIX: D October 14, 2004 Permit to construct Waiver - SVE System

tile: Burley I Ha



1410 North Hilton • Boise, Idaho 83706-1255 • (208) 373-0502

Dirk Kempthorne, Governor Toni Hardesty, Director

October 14, 2004

Certified Mail No. 7000 0520 0016 0850 2864

Mark Petersen, Manager of Pipelines and Terminal Sinclair Oil Corporation P.O. Box 30825 Salt Lake City, Utah 84139

RE:

Facility ID No. 031-00026, Sinclair Oil Corporation, Burley

Permit to Construct Exemption - SVE

Dear Mr. Petersen:

On September 30, 2003, the Idaho Department of Environmental Quality (DEQ) received notification regarding the expansion of operations of the soil vapor extraction (SVE) unit at its Burley terminal. Based on review of the submitted materials and all applicable state and federal rules and regulations, DEQ has determined that the project still meets the permit to construct exemption requirements in accordance with IDAPA 58.01.01.220 through 223 (Rules for the Control of Air Pollution in Idaho). Therefore, a PTC is not required for this project.

This letter is in no way intended to supersede any other federal, state, or local rules and regulations that may apply. Also, be advised that this letter does not constitute a waiver of any compliance actions that may result from misinformation or noncompliance of the criteria set in the submittal received for this project that may cause unreasonable risk to human or animal life, or violate any ambient air quality standard.

If you have any questions regarding this letter or about the air quality permitting process, please contact Bill Rogers at (208) 373-0502.

Sincerely,

Martin Bauer, Administrator

Maita Bacc

Air Quality Division

MB/ABC/sd

Project No. X-040413

Steve VanZandt, Twin Falls Regional Office
 Almer Casile, Permit Writer
 Bill Rogers, Permit Coordinator
 Laurie Kral, Region 10 USEPA



Air Quality Permitting Statement of Basis

October 7, 2004

Permit to Construct No. X-040413

Sinclair Oil Corporation, Burley

Facility ID No. 031-00027

Prepared by:

Almer Casile, Permit Writer AIR QUALITY DIVISION

Permit to Construct Exemption Concurrence

Table of Contents

AC.	RONYMS, UNITS, AND CHEMICAL NOMENCLATURES	3
l.	PURPOSE	., 4
2.	FACILITY DESCRIPTION	4
3.	FACILITY / AREA CLASSIFICATION	., 4
4.	APPLICATION SCOPE	. 4
5.	PERMIT ANALYSIS	. 4
6	RECOMMENDATION	6

Acronyms, Units, and Chemical Nomenclatures

acfm actual cubic feet per minute
AFS AIRS Facility Subsystem

AIRS Aerometric Information Retrieval System

AQCR Air Quality Control Region

ASTM American Society for Testing and Materials

CAA Clean Air Act

cfm cubic feet per minute

CFR Code of Federal Regulations

CO carbon monoxide

DEQ Department of Environmental Quality
EPA U.S. Environmental Protection Agency

HAPs Hazardous Air Pollutants

IDAPA a numbering designation for all administrative rules in Idaho promulgated in accordance

with the Idaho Administrative Procedures Act

lb/hr pound per hour

MACT Maximum Achievable Control Technology

NESHAP National Emission Standards for Hazardous Air Pollutants

NO_X nitrogen oxides

NSPS New Source Performance Standards

 O_3 ozone

PM particulate matter

PM₁₀ particulate matter with an aerodynamic diameter less than or equal to a nominal 10

micrometers

PSD Prevention of Significant Deterioration

PTC permit to construct
PTE potential to emit

Rules Rules for the Control of Air Pollution in Idaho

SIC Standard Industrial Classification

SIP State Implementation Plan

 SO_2 sulfur dioxide T/yr tons per year

UTM Universal Transverse Mercator VOC volatile organic compound

PURPOSE

The purpose for this memorandum is to satisfy the requirements of IDAPA 58.01.01.200, Rules for the Control of Air Pollution in Idaho, for issuing permits to construct.

2. FACILITY DESCRIPTION

Sinclair Oil Corporation (Sinclair), in conjunction with Chevron Pipeline, Tesoro Petroleum Companies operates a petroleum products storage facility at the Burley Product Terminals in Burley. The equipment in this project includes a SVE system that is used to remove hydrocarbons from contaminated soil.

3. FACILITY / AREA CLASSIFICATION

The facility is a major facility as defined by IDAPA 58.01.01.008.10 because the facility's potential to emit for VOC is greater than or equal to 100 T/yr. The facility is not a major facility with regard to HAP emissions. The facility is not a designated facility as defined by IDAPA 58.01.01.006.27.

The facility is located within AQCR 63 and UTM zone 12. The facility is located in Cassia County, which is designated as unclassifiable for all criteria pollutants.

The AIRS information provided in Appendix B defines the classification for each regulated air pollutant at the facility. This required information is entered into the EPA AIRs database.

4. APPLICATION SCOPE

Sinclair Oil Corporation (Sinclair), in conjunction with Chevron Pipeline, Tesoro Petroleum Companies is proposing to expand operations of the soil vapor extraction (SVE) system at the Burley Product Terminals in Burley. Sinclair seeks concurrence of its SVE system self-exemption as it pertains to DEQ's Guidance For Remediation Of Petroleum Contaminated Media.

4.1 Application Chronology

September 30, 2004 DEQ received notification of expansion of the SVE system from Sinclair's consultant Maxim.

5. PERMIT ANALYSIS

This section of the Statement of Basis describes the regulatory requirements for this PTC action.

5.1 Equipment Listing

The equipment in this project includes a SVE system that is used to remove hydrocarbons from contaminated soil. The facility has installed additional soil vapor recovery points, modified the piping manifold to the handle the additional points, and extended the trunk line from the manifold to the vacuum source for the SVE. (See Appendix A for additional information.)

5.2 Emissions Inventory

The applicant tested for the VOC and benzene concentration in the effluent stream. The results of the tests show a benzene concentration of $2\mu g/liter$ and a VOC concentration of $1100\mu g/liter$. The flow rate through the SVE system is 500 cubic feet per minute (cfm). Using SVE policy calculations, the resulting benzene and VOC emissions estimates are 0.09 lb/day and 9.02 T/yr, respectively.

5.3 Modeling

Since the benzene lb/day emissions are less than the 0.192 lb/day (which includes the short-term source factor as defined in IDAPA 58.01.01.210.15) as provided in DEQ's SVE policy, no modeling is required.

5.4 Regulatory Review

The self-exemption, as submitted by the facility, has satisfied the following guidance requirements:

- 1. Petroleum remediation only (not industrial solvents or other remediation projects).
- 2. Annual uncontrolled VOC emissions are estimated to be less than 100 tons per year (IDAPA 58.01.01.220.01.a.i).
- 3. For major sources, annual uncontrolled VOC emissions are estimated to be less than 40 tons per year (IDAPA 58.01.01.220.a.ii).
- 4. Not part of a new major facility or part of a proposed major modification (IDAPA 58.01.01.220.01.b).
- 5. An operational life of no more than five years (not for landfills) (IDAPA 58.01.01 006.34).
- 6. As can be determined from the submittal, the source is not located near a sensitive receptor.
- 7. Estimated benzene emissions are less than or equal to 0.192 lb/day (which includes the short-term source factor. Therefore, no control equipment and no minimum stack height is required.

5.5 Fee Review

No application fee or processing fee was required in accordance with IDAPA 58.01.01.224-225 because this project is for a permit to construct exemption concurrence.

	Emissions Ir	iventory	
Pollutant	Annual Emissions Increase (T/yr)	Annual Emissions Reduction (T/yr)	Annual Emissions Change (T/yr)
NO_X	0.0	0	0.0
SO ₂	0.0	0	0.0
CO	0.0	0	0.0
PM ₁₀	0.0	0	0.0
VOC	0.0	6.88	6.88
TAPS/HAPS	0.0	0	0,0
Total:	0.0	0	0.0
Fee Due	\$ 0		

(8) 1.1 (7.1.17) 1.1 (1.1.17)

6. RECOMMENDATION

Based on review of application materials and all applicable state and federal rules and regulations, staff concur that this project is exempt from permit to construct requirements

ABC/sd Permit No. X-040413

G:\Air Quality\Stationary Source\SS Ltd\Exempt\Sinclair Burley\X-040413\X-040413 SB.doc

APPENDIX A

Facility Exemption Concurrence Request & Emission Inventory

Shawnee Chen

From:

Patricia Rayne

ent:

Thursday, October 19, 2006 8:54 AM

10:

William Rogers; Shawnee Chen; Stephen Vanzandt

Cc:

Marilyn Seymore; Phyllis Heitman; Betty Flowers; Sherry Davis; Patricia Rayne

Subject:

RE: New projects - Sinclair Transportation, Burley - Change in Permit #

Follow Up Flag: Follow up

Flag Status:

Red

See below: the Tier 2 permit # should be T2-060446

From: Patricia Rayne

Sent: Tuesday, October 17, 2006 10:57 AM

To: William Rogers; Shawnee Chen; Stephen Vanzandt

Cc: Marilyn Seymore; Patricia Rayne; Phyllis Heitman; Betty Flowers; Sherry Davis

Subject: New projects - Sinclair Transportation, Burley

New permitting projects:

T1-060445 Sinclair Transportation Company 031-00026 Received 10/12/06 T1 Renewal

Shawnee Chen assigned.